



Heat transfer – a review of 2000 literature

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1. Introduction

Heat transfer continues to be a major field of interest to engineering and scientific researchers, as well as designers, developers, and manufacturers. The wealth of applications includes a wide variety of components and systems for energy devices, including general power systems, heat exchangers, high performance gas turbines and other power conversion devices. Other areas of interest include chemical processing, general manufacturing, bio-heat transfer, electronic cooling, comfort heating and cooling, and a number of natural phenomena from upwelling currents in the oceans to heat transport in stellar atmospheres.

The present review is intended to encompass the English language heat transfer papers published in 2000. While being exhaustive, some selection is necessary. Many papers reviewed herein relate to the science of heat transfer, including numerical, analytical and experimental works. Others relate to applications where heat transfer plays a major role in not only virtually all man-made devices, but natural systems as well. The papers are grouped into categories and then into sub-fields within these categories. We restrict ourselves to papers published in reviewed archival journals.

Besides reviewing the journal articles in the body of this paper, we also mention important conferences and meetings on heat transfer and related fields, major awards presented in 2000, and books on heat transfer published during the year.

The 34th National Heat Transfer Conference on 20–22 August in Pittsburgh, USA had sessions on enhanced

heat transfer in heat exchangers, microscale transport phenomena, heat transfer in electronic systems, inverse problems and porous media. The ASME International Mechanical Engineering Congress and Exposition (IMECE-2000) was held in Orlando, USA on 15–20 October. The Heat Transfer Division of the ASME organized sessions on heat transfer in turbomachinery, heat transfer enhancement in multiphase flow, CFD in multi-dimensional two-phase flows, transport phenomena in materials processing, and radiative heat transfer. The ASME Turbo Expo ‘Land, Sea and Air-2000’ held in Munich, Germany had sessions on film cooling and blade internal and external heat transfer.

A Symposium on Energy Engineering was conducted in 9–12 January in Hong Kong; sessions covered forced convection, air-conditioning and refrigeration, boiling and condensation, and clean combustion technology. The Fourth ISHMT/ASME Heat and Mass Transfer Conference was held on 12–14 January in Girinagar, India. The 5th International Workshop on Advanced Plasma Tools and Process Engineering was held on 10–11 February in Santa Clara, USA. The Eighth International Seminar on Numerical Combustion was held on 5–8 March in Amelia Island, USA. The Third International Symposium on Turbulence Heat and Mass Transfer was organized on 3–7 April in Nagoya, Japan. The 4th Minsk International Heat and Mass Transfer Forum on 22–26 May discussed issues in heat and mass transfer in disperse and rheological systems and capillary-porous bodies. An ASME-ZSIT International Thermal Science Seminar was held on 11–14 June in Bled, Slovenia. The Eurotherm Seminar N64 held on 18–21 June in Reims, France covered advances in quantitative infrared thermography. The 14th Symposium on Thermophysical Properties was held on 25–30 June in Boulder, USA. The Sixth International Conference on Advanced Computational Methods in Heat

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Transfer was held in Madrid, Spain on 26–28 June. Papers were presented on natural and forced convection, porous media and composites, inverse problems, coupling of different numerical methods, and heat transfer in manufacturing.

The 7th Australasian Heat and Mass Transfer Conference was held on 3–6 July in Townsville, Australia; topics covered, among others, were combustion, conduction, multiphase flow and computational methods. An International Symposium on Heat Transfer in Gas Turbine Systems was held on 13–18 August in Cesme, Turkey; sessions covered disk cavity and blade heat transfer, combustor liner cooling, film cooling and internal cooling. The 4th ASME–JSME Thermal Engineering Conference was held in Kobe, Japan on 1–6 October; topics covered included phase change, flow in microgravity, and microscale heat transfer. The International Symposium on Multiphase Flow and Transport Phenomena (MFTP-2000) held on 5–10 November in Antalya, Turkey covered bio-aerosols and bio-systems, surface and interfacial phenomena, pollution control and cleanroom technology, and scaling laws for two-phase phenomena.

In 2000, the 1999 Max Jakob Award was bestowed on Adrian Bejan for his pioneering work on entropy generation minimization and exergy analysis and his lifelong contributions to the areas of natural convection, porous media, and combined heat and mass transfer. The Donald Q. Kerby award was given to V.K. Dhir for his outstanding applied research contributions to phase change and thermal hydraulics of nuclear systems, and basic and applied research contributions in heat and mass transport. At IMECE-2000, the Heat Transfer Memorial Awards were presented to Ramesh Shah (Art) for his significant contributions to the design theories of compact heat exchangers and education worldwide through lectures, Dr. Ashley Emery (General) for demonstrating the importance of heat transfer fundamentals in a wide spectrum of research and engineering applications, and Dr. Ta-Shen Chen (Science) for outstanding pioneering contributions to the understanding of mixed convective heat transfer, instability mechanisms, and transport processes in such flows.

Books published during the year on heat transfer include:

Advances in Enhanced Heat Transfer
ASME Press

Advanced Computational Methods in Heat Transfer
B. Sunden, C. Brebbia

Advances in Heat Transfer, Vol. 34
J.P. Harnett, T.F. Irvine, G.A. Greene
Academic Press, Inc.

Advances in Numerical Heat Transfer
W.J. Minkowycz, E. M. Sparrow (editors)
Taylor & Francis

Condensation Heat Transfer Enhancement
V.G.G. Rifert, H.F. Smirnov

Computational Analysis of Convection Heat Transfer
G. Comini, B.Sunden (editors)
Computational Mechanics, Inc.

Dynamics of Regenerative Heat Transfer
J.A. Wilmott
Taylor & Francis

Extended Surface Heat Transfer
A.D. Kraus, A. Aziz
John Wiley and Sons

The Finite Element Method in Heat Transfer and Fluid Dynamics
J.N. Reddy, D.K. Gartling
CRC Press

The Finite Analytic Method in Flows and Heat Transfer
C.J. Chen, R.A. Bernatz, W. Lin, K. Carlson
Computational Mechanics, Inc.

Fundamentals of Momentum, Mass and Heat Transfer
J.R. Welty, R.E. Wilson, C.E. Wicks, G.L. Rorrer
John Wiley and Sons

Fundamentals of Heat and Mass Transfer
F. Incropera and D.P. DeWitt
John Wiley and Sons

Heat Transfer
V.P. Isachenko, S. Semyonov, A. Sukomel
University Press of the Pacific

Heat and Mass Transfer Under Plasma Conditions
P. Fauchais, J. Heberlein, J. van der Mullen (editors)
New York Academy of Sciences

Proceedings of the International Conference on Heat Transfer and Transport Phenomena in Microscale
G.P. Celata, V. P. Carey (editors)
Begell House Publishers, Inc.

Heat Transfer in Industrial Combustion
C. Baukal
CRC Press

Heat Transfer
L.C. Thomas
Capstone Publishing Corporation

Introduction to Heat Transfer
V. Arpaci, A. Selamet, S.-H. Kao
Prentice-Hall

Introduction to Heat Transfer
F. Incropera and D.P. DeWitt
John Wiley and Sons

Modelling of Transport Phenomena in Crystal
Growth
J.S. Szmyd, K. Suzuki (editors)
Computational Mechanics, Inc.

Microgravity Fluid Physics and Heat Transfer
International Conference on Microgravity Fluid
Physics and Heat Transfer
Begell House Publishers, Inc.

National Heat Transfer Conference Proceedings
American Nuclear Society

Principles of Heat Transfer
F. Kreith, M. Bohn
Brooks/Cole Publishing Company

Radiation Heat Transfer
H.R.N. Jones
Oxford University Press

2. Conduction

The category related to Heat Conduction always enjoys widespread research activity in various sub-topics to include: Contact conduction and contact resistance; Composites and Heterogeneous media; Heat conduction in solids of arbitrary geometries; Thermal waves and micro/nanoscale heat transfer; Conduction with convection and flow effects; Thermomechanical problems; Materials and modeling; Analytical, Numerical and Experimental Studies; and Miscellaneous studies in heat conduction. The various efforts in each of the sub-categories are highlighted next.

2.1. Contact conduction and contact resistance

Contact conductance measurements under high temperature across a cylindrical joint by a periodic method [1A]; metal polymer joints [2A]; enhancement of contact conductance and effect of metallic coating [3A]; analysis of heat transfer in film covered composite–steel surfaces [4A] and gap conductance due to contact heat transfer [5A] have appeared in this sub-category.

2.2. Composites and heterogeneous media

Specific studies dealt with experimental investigations of resistance welding in thermoplastic-composites [6A]; axisymmetric transient solutions in layered composites

[7A]; experimental/numerical studies of residual stresses [8A]; macro/micro periodic layered solids [9A]; transient analysis in 1-D slab [10A]; thermal diffusivity measurements in composites with thick fillers and rubbers [11A]; thermal resistance on heat transfer in composite medium using thermal wave model [12A]; and thermo-hygro-mechanical tailoring of composites accounting for second sound [13A].

2.3. Heat conduction in arbitrary geometries

The various issues dealing with pin fins [14A], T-shaped fins [15A], heat-pipe fin [16A], extended heat transfer fins [17A], binary mixtures of granular materials [18A], irregularly spaced plane strip contact [19A], and modeling of transient conduction in plane slabs employing a rational method for distribution of nodes [20A] appear in this sub-category.

2.4. Thermal waves, micro/nanoscale effects, and laser heating

This sub-category is receiving widespread research interest and an increased emphasis in various issues dealing with thermal waves and hyperbolic nature of heat transport, prediction of thermophysical properties in micro/nanoscale sizes, analytical and numerical analysis of thermal propagation and distribution appear in various indepth studies in [21A–35A].

2.5. Conduction with convection and flow effects

The transient analysis of a 2-D cylindrical pin with constant base heat flux and tip convective effects appeared in [36A].

2.6. Thermomechanical problems and applications

The thermoelastic stress analysis to fully reversed bending fatigue [37A], composites under local intense heating by irradiation [38A], continuous casting processes [39A], an efficient approach to computing residual stresses in welded joints [40A], and residual stresses in aluminum alloy forgings [41A] appeared in this sub-category.

2.7. Materials and modeling

The process of cure during repair of a broken thermoset piece by heating with a new uncured resin [42A], finite gap effects on modeling thermal contact conductance at polymer–mold wall interface [43A], distortion induced by electron beam welding [44A] for a nickel-based superalloy, and a model for conduction through oxide layer of steel during hot rolling [45A] appeared in this sub-category.

2.8. Analytical, numerical and experimental studies

Various issues ranging from developing new analytical tools and numerical simulations for a broad range of heat conduction applications appeared in the literature. In certain applications experimental studies were either additionally undertaken or results of experiments were provided for selected applications. The numerical simulations either employed new and novel techniques and/or use of existing tools for varied applications. All these appeared in [46A–65A].

2.9. Miscellaneous studies

As always, numerous studies appeared in the literature for problem specific and selected applications that addressed the aspects of heat conduction. The various details of these miscellaneous topics appeared in [66A–80A].

3. Boundary layers and external flows

Papers on boundary layers and external flows for 2000 have been categorized as follows: flows influenced externally, flows with special geometric effects, compressible and high-speed flows, analysis and modeling techniques, unsteady flow effects, flows with film and interfacial effects, flows with special fluid types and property effects and flows with reactions.

3.1. External effects

Papers which focus on external effects document the influence of blowing or suction through the wall [1B–3B,5B,9B,11B], adverse pressure gradients [6B], free-stream turbulence [8B], electric fields [7B], magnetic fields [4B,10B] and viscosity's dependence on temperature [12B].

Several papers include studies of injection or suction through porous walls. In one, heat transfer is enhanced by injection-induced turbulence effects [5B], another applies suction to a stretching sheet of variable conductivity [1B], a third is similar, but with a visco-elastic fluid [2B], the fourth is with another non-Newtonian fluid [11B], the fifth investigates the effects of nearness to the exit of the extrusion slot on the local heat transfer characteristics [3B] and the final is with a compressible laminar flow on a wall [9B]. In [9B], injection through multiple slots is shown to move the point of separation downstream. Separation moves upstream when suction is applied. The effects of adverse pressure gradient over a 2-D boundary layer on mass transfer in compressible flow are presented as a means of control [6B]. The effects of free stream turbulence level on turbulent boundary layers are discussed in [8B]; substantial augmentation of

heat transfer with elevated turbulence is computed. The effects of an electric field on mass transfer from a liquid drop are discussed in [7B]; mass transfer enhancement is strong when operating at an optimum frequency. The influence of a magnetic field on mass transfer from a stretching sheet is described in [10B] where it is noted that the skin friction is strongly increased while the heat transfer is only slightly reduced. Another paper describes the effects of a magnetic field on heat transfer from a plate cooled by a non-Newtonian fluid [4B]. Finally, the sensitivity of viscosity to changes in temperature is capitalized upon in a strategy for active control of fluctuations in surface heat flux [12B].

3.2. Geometric effects

Papers in this category address heat transfer in several geometries; a moving surface [15B,29B,33B], spheres, wedges and geometrically similar objects [19B, 20B,23B, 27B,28B], wavy, rough and ribbed surfaces [16B,17B, 21B,25B,26B,30B,31B,34B], airfoils [18B,32B], stagnation flows [13B,14B], flows in a room [35B] and flows with strong shear [22B,24B].

Several papers dealt with moving surfaces. One [15B] simulates casting or rolling processes and another, with Newtonian fluids and pseudo-plastics, discusses heat transfer in extrusions [29B]. On a larger scale, a paper is presented which deals with the energy, mass and momentum transfer in moving viscous mantle-solid systems representing continents [33B]. Heat transfer from geometrically similar objects is analyzed in [27B] and heat transfer from wedges in [19B,20B,23B]. In the latter two, the wedge surface is permeable. Wavy surfaces with micro-polar fluids are treated in two similar papers [16B,17B]. Three papers deal with roughness; in one [34B], curvature effects are included; in another, the wall is permeable and the Reynolds analogy is addressed [31B] and, in a third [25B], variational methods are used to estimate aerodynamic roughness length. The effects of ribs mounted on a surface are discussed in [26B], based on results from RANS modeling techniques; while in another [21B], heat transfer performance with detached and attached ribs is compared. Another similar paper shows computed heat transfer from surfaces with protruding bodies [30B]. It notes the importance of activating the unsteady term in the equations. Two airfoil studies are included; in one [32B], an unsteady compressible code is applied to compute conjugate heat transfer in a turbine blade. In another [18B], the geometries of iced airfoils are used, noting the differences between rime and glazed ice behavior. Two flows with stagnation heat transfer are presented, one at the stagnation point on a wall [13B] and another in a jet impingement geometry [14B]. In the latter, the effects of inlet chamfering of the delivery hole are addressed. Other papers in this category include large eddy simu-

lation of natural and forced convection heat transfer in a room [35B], the turbulent thermal boundary layer of the entry flow to a channel [24B] and transfer of a passive species in a shear flow [22B].

3.3. Compressibility and high-speed flow effects

Papers in this category include two on blunt leading edges [39B–41B], two on non-equilibrium effects [36B, 42B], one on slip velocity effects [43B] and two on modeling [37B, 38B].

An artificially blunted leading edge is shown to have reduced drag [39B]. The effects on heat transfer of such leading edge changes are documented. Non-equilibrium effects on a blunt body in hypersonic flows are discussed [41B] where the effects of vibrational temperatures on heat flux and shock standoff distance are described. Experiments in transonic and supersonic flows with plasma and hot gas injection document the drag reduction effect [36B]. The effects of thermochemical non-equilibrium on shock standoff distance for high-speed flow around a sphere are measured [42B]. Another paper presents an analysis of the effects of slip velocity on heat transfer and condensed phase momentum flux of a supersonic nozzle flow [43B]. The application is industrial cleaning. Direct numerical simulation is applied to supersonic turbulent boundary layers [38B]. The modeling choices are discussed. Finally, a research group reported over-prediction of heat transfer in hypersonic flows [37B]. They attribute it to shortcomings in turbulence modeling.

3.4. Analysis and modeling

Papers in this category include some on modeling of turbulence in Reynolds-averaged equations [44B–46B, 48B, 54B, 56B, 57B, 59B], some focus on near-wall modeling, others present DNS and LES simulation techniques [49B, 52B, 53B], two are on transition [47B, 51B], one is on the Reynolds analogy factor [50B] and two present modeling of atmospheric flows [55B, 58B].

A turbulent heat flux transport model is proposed and tested against DNS and experimental results in homogeneous turbulence [46B]. A homogeneous turbulent shear flow is used to discuss the evolution of passive scalar fields [57B]. Anisotropic RANS modeling of the $k-\varepsilon-A$, three-equation eddy viscosity type is shown to be encouraging in capturing anisotropic behavior in thermal fields [45B]. A survey of various RANS models applied to heat transfer in wood heaters is presented [48B]. Near-wall turbulence modeling is addressed as applied to Reynolds-averaged energy equation modeling [44B]. A low-Reynolds number model is applied to pipe entry flow where three variations on turbulent Prandtl number modeling are employed [54B]. Near-wall modeling is addressed in a two-equation RANS model

leading to the suggestion that the temperature-field model must be at least one level lower in order than the velocity-field model [56B]. A wall function is discussed for application to computing with variable-property fluids and permeable surfaces [59B]. Near-wall modeling using DNS is discussed for fluids of various Prandtl numbers. A new dynamic subgrid-scale turbulence model is presented for use in LES computation of turbulent stress and heat flux fields [49B]. Subgrid-scale modeling of atmospheric boundary layers is discussed in terms of stability and filter dimensions [53B]. Transition to turbulence in high-speed flows is computed by assuming that non-turbulent fluctuations behave in a turbulent-like manner [51B]. Time-dependent calculations of wake-affected flows which use an intermittency function to effect transition are shown to be superior to computations made with quasi-steady assumptions. The Reynolds analogy factor, St/Cf , is used to discuss thermal convection driven by non-isothermal stretching surfaces [50B]. A model is presented for including sensible and latent heat fluxes in atmospheric boundary layers [58B]. It is used to compute vapor transport from the surface of the Bay of Bengal. Also, for atmospheric flow, a dissipation integral is applied to compute surface fluxes [55B].

3.5. Unsteady effects

Flows in this category include one which tests a quasi-static hypothesis [62B], two for flat-plate boundary layers [61B, 69B], one which compares timescales [66B], one on drag reduction strategies [70B], four on heat transfer to spheres [60B, 64B, 65B, 68B], one for wake effects [63B] and two on flow stability [67B, 71B].

A numerical study of transient cooling with variable fluid viscosity is presented [62B], showing that a convective onset time can be scaled on a viscous temperature scale. Conjugate heat transfer is applied to a flat-plate flow to evaluate surface temperature evolution [61B]. An analysis is applied to an impulsively started flat plate [69B]. The results of limiting cases are compared to exact solution results. Measurements are made of the turbulent concentration variance and its dissipation [66B] in support of experimentally evaluating the scalar-to-velocity timescale ratio. Coherent structures are computed with DNS to discuss strategies for drag reduction [70B]. Transient heat transfer to particles is computed for various Reynolds and Peclet number values [64B]. Results show a strong sensitivity to Re when Pe values are above unity. The effects of flow pulsation on particle heat transfer are described experimentally [68B]. Heating of liquid droplets in immiscible fluids is computed and the effects of Reynolds number and the effects of the ratio of external to internal viscosity are quantified [60B]. The effects of acoustic excitation on heat transfer from a bubble are evaluated and the results are compared to

magnetic excitation effects [65B]. Transient heat transfer to airfoils, as affected by passing wakes, is described [63B]. Transitional spot spreading and propagation rates are documented experimentally by using liquid crystal thermometry [71B]. Finally, the development of compression and gravity waves, their growth and decay, in convective storms is described [67B].

3.6. Films and interfacial effects

Papers in this category address droplet evaporation [76B], direct contact heat exchangers [77B], falling films [72B–74B,79B], co-current and counter-current flows [75B] and instability [78B].

A paper on droplet evaporation numerically investigates the interaction among droplets. Groups of droplets behave differently than single droplets [76B]. The direct contact heat exchange between perfluorocarbons and hot water is experimentally evaluated [77B], describing the effects of size distribution and flow behavior. The effects of humidity on the thermocapillarity of a falling film are addressed [79B]. Liquid film heat transfer for heat exchangers operating under various Peclet number conditions is analyzed [73B]. A mathematical model is presented for an ammonia–water falling film to describe the effects of subcooling and initial film thickness [74B]. A similarity transformation is employed to analyze a laminar liquid film on a horizontal stretching sheet [72B]. In the limit of high Pr , the film surface temperature is shown to approach that of the sheet. A similarity variable method is employed to describe mass transfer across the interface in co-current and counter-current flows [75B]. The advantages of using co-current flows are presented. Finally, the Rayleigh–Taylor stability of vapor–liquid interfaces is studied [78B] by use of a multiple-timescale expansion method.

3.7. Effects of fluid type or fluid properties

Papers in this category include one with a heat generating fluid [80B], one in the Knudsen transition range [82B], two with particles in a gas [83B,85B] and one on the earth's mantle [81B].

A theoretical study describes the solidification of a heat-generating fluid [80B]. Correlation with a modified Rayleigh number is given. Non-continuum heat transfer between isolated, motionless, highly overheated spherical particles and the cooler surrounding gas is studied by a Monte Carlo simulation [82B]. Equations for accurate estimates of the heat transfer coefficients with temperature-dependent heat capacities are given. Direct numerical simulation is used to compute fluid and particle temperature decay in isotropic turbulence [83B]. A Lagrangian random-walk simulation is used to compute thermophoretic transport in a particle-laden flow [85B]. The relative importance of the various mechanisms is

discussed and results for mass deposition rates are compared with experiments. Stagnation point flow of dissociated carbon dioxide is measured [84B]. The effectiveness values of various catalysts of the process are evaluated, showing silver to be the best catalyst. Flow dynamics and heat transfer of 3-D mantle convection are computed [81B]. Variable thermal conductivity is found to stabilize the flow greatly. The authors suggest that plume-like structures observed by others may be manifestations of this nonlinearity in the conductivity.

3.8. Flows with reactions

Papers in this category include one on reacting jets [88B], one with a flame on a cooled wall [87B], two on wall deposition rates [89B,90B] and another dealing with high-speed flow [86B].

The effects of dispersion characteristics on particle temperatures in a non-premixed reacting jet are evaluated [88B]. This is done by a parametric study using a Lagrangian simulation, where the continuous phase is computed with DNS. It is found that the particle temperature behavior is a strong function of spatial dispersion. The effects of wall boundary conditions are evaluated for hydrogen flames over various surfaces [87B]. Boundary conditions described are: a cooled wall, a catalytic surface and an inert surface. A mathematical model is formulated for computing the growth of a product layer of a bimolecular reaction on a reactor wall [89B]. The role of the reactor design is discussed. The growth rate of a diamond layer is predicted with a 2-D model written to describe the hydrodynamics and chemistry of the process [90B]. Though some experimental results are computed accurately, some discrepancies were noted and a tie is made to the use of the Miller–Melius mechanism model for rich oxy-acetylene flames. Numerical simulations of high-speed flow of a high-temperature, non-equilibrium reacting gas mixture over a flat plate are made [86B]. With a kinetic scheme, which allows partial recombination in the boundary layer, good agreement with experiments is found.

4. Channel flows

4.1. Straight-walled ducts

Straight-walled ducts with a variety of cross-sectional geometries are reviewed in this section. Heat and mass transfer for turbulent flow in circular tubes with uniform wall temperature was addressed using a resistance-in-series model [2C]. The forced-convection of slug flow was examined in a rectangular duct [3C]; rectangular ducts were also studied with constant axial heat flux [15C,16C]. Experiments investigated the laminar mixed convection of an inclined duct; buoyancy assisted and

opposed conditions were considered [5C]. Mixed convection was also studied using linear stability of purely convective Poiseuille flow [17C], and to address Prandtl number effects in vertical pipes [22C]. The modeling of turbulence and relaminarization of forced gas flows at high-heat flux was undertaken [18C]. A low-Reynolds number algebraic stress model was examined for turbulent flow under fully developed conditions [19C]. Strong heating was also modeled for the laminarization of gas flows in circular tubes [21C]. Flow and heat transfer in annular-sectored ducts was studied both experimentally [23C] and numerically [12C]. Thermal stresses were investigated in fully developed laminar flow conditions [1C]. A large number of low Reynolds number $k-\epsilon$ models were compared for turbulent pipe flows [24C]. Heat transfer in triangular ducts was studied for different apex angles using the SIMPLE method [6C]. The optimum cross-sectional geometry for maximum heat transfer for a given pressure loss was evaluated at constant wall temperature [25C]. Buoyancy-assisted flow separation was modeled using a modified FLARE procedure [7C]. Inclined cooling ducts were examined for determining the heat transfer characteristics for the design of PV cooling ducts [4C]. Buoyancy-assisted flow was studied in the entrance region of a vertical rectangular duct [8C]. The Integral Transform Technique was used to study the turbulent heat transfer characteristics of drag-reducing fluids [13C]. The influence of rarefaction on heat transfer in circular tubes was studied [11C] as well as the thermomechanical coupling in Couette flow [9C]. An analytical study was undertaken to understand the entropy generation in turbulent liquid flows in smooth ducts with constant wall temperature [20C]; an entropy production theorem was used to investigate the performance of enhanced heat transfer surfaces in ducts with constant wall temperature [26C]. The heat transfer to liquid lithium was examined when exposed to a transverse magnetic field [14C]. The effect of Lorenz force in the flow of conducting turbulent fluids was also studied [10C].

4.2. Microchannel heat transfer

Recent attention to micro-scale phenomena has led to an increase in papers devoted to microchannel heat transfer. Heat transfer in a silicon substrate containing rectangular microchannels was investigated numerically [27C]. The 3-D conjugate heat transfer was studied in the microchannel heat sink [29C]. Wall effects on the heat transfer behavior was examined in laminar gas flows [30C]. Irregular cross-sections were considered for low Reynolds number microchannel flows [32C]. Scale effects were used to study differences in microchannel and large-scale channel heat transfer [33C]. The heat transfer of water flow in trapezoidal microchannels was studied experimentally [31C]. Vapor–liquid flow was

studied in a micro-heat pipe; the phase change process was examined numerically [34C]. Heat transfer characteristics were investigated in the microchannels of thermal conductivity detectors; boundary conditions, channel size and property effects were considered [28C]. Surface radiation in an annular enclosure was studied numerically for meniscus-driven convection [36C]. Experiments were conducted to evaluate the importance of Brinkman number in microchannel heat transfer [35C].

4.3. Irregular geometries

Forced-convective heat transfer was investigated in curved channels for laminar conjugate conditions [40C]. Local heat transfer measurements were made near a 180° turn in a rectangular channel [37C]. A numerical study considered the laminar to transitional range of Reynolds numbers in corrugated ducts; both heat transfer and pressure drop results are presented [39C]. Flow visualization using liquid crystals was used to examine the local heat transfer characteristics near a 180° bend of a two-pass square duct [44C]. A reduced equation is presented to assist in the calculation of the heat transfer and temperature distribution on the surfaces of square and non-square internal turbine blade cooling channels [51C]. Flow and heat transfer in helically coiled pipes was examined to determine the roles of curvature and torsion [43C] as well as the conjugate problem of a coil immersed in a chilled water container [46C]. The effect of inlet conditions on the flow and heat transfer in endwall secondary flows was computed and compared to experiment [41C]. The cooling of a volume experiencing heat generation at all locations was studied for parallel-plate channels and round tubes [38C]. The inverse force convection problem was investigated in a 3-D irregular duct; the effects of duct height, inlet fluid velocity and measurement errors were considered [42C]. The thermal hydraulic analysis of cable-in-conduit-conductors was modeled numerically [53C]. The slow flow of liquid in conical annular channels was solved by separation of variables [50C]. Experiments were used to obtain instantaneous heat fluxes in cylinder heads and exhaust manifolds [47C]; load and speed effects were also considered [48C]. A heat-pipe cooled piston crown was studied experimentally to provide effect means for piston temperature control [52C]. Heat sources modeled as Dirac delta functions used to investigate the performance of flat-plate heat pipes [49C]. Experiments were used to study the thermal behavior of an asymmetrical flat-plate heat pipe [54C]. Mixed convection was modeled in the windings of a disc-power transformer [45C].

4.4. Finned and profiled ducts

Extended surfaces, protrusions, twisted elements and other surface enhancements in channel flows are

considered in this section. Turbulent heat transfer was studied in a wavy channel having twisted tape elements and interrupted ribs; averaged heat transfer distributions and friction factors were obtained [80C]. The 3-D hydrodynamically and thermally developing laminar flow and conjugate heat transfer in oval tubes were calculated [55C]. The effects of property variations and buoyancy were considered for laminar flow in tubes with twisted tape inserts [57C]. The heat transfer of laminar flow in channels with corrugated walls was studied using a numerical model [59C]. The performance of asymmetrical longitudinal fins in annular ducts was optimized for laminar flow conditions [60C]. The heat transfer on the annulus side of a spirally fluted tube was studied to examine the effect of fluid property variations [62C]. Slots were used to enhance the heat transfer in channels with surface mounted blocks [64C]. The laminar flow in vertical pipes with twisted tape inserts was investigated experimentally; the flow of water in air-cooled copper pipes was considered [65C]. Experiments were used to study the flow of water, ethylene glycol and turbine oil through tubes with internal extended surfaces and continuous and segmented twisted-tape elements [69C,70C]. Heat transfer enhancement in a circular duct with circumferential fins and circular disks was studied experimentally for fully developed turbulent flow [74C]. Periodic ribs were used to enhance the turbulent heat transfer in a channel and were modeled numerically [76C]. A numerical method was also used to study the laminar flow in an air-cooled horizontal printed circuit board [67C]; heat transfer from multiple protruding heat sources simulating electronic components was addressed in the laboratory [75C]. An experimental investigation was undertaken to study the forced convection in air-cooled, horizontal, equilateral-triangular ducts [68C]. Heat transfer measurements were made inside straight and tapered two-pass channels with rib turbulators to model the characteristics in gas turbine blade passages [58C]. Spirally corrugated tubes and inlet axial vane swirlers were used to enhance heat transfer in channels; experimental results are presented [79C]. A square ribbed duct was examined numerically using a low Reynolds number turbulence model together with a simple eddy viscosity model and an explicit algebraic stress model [72C]. Multilobe vortex generators were used to enhance heat transfer in a circular tube; a finite volume method was used [77C]. Solid and perforated blocks attached to the flat plates in ducts were compared to the plate performance without the enhancement [73C]. The cooling of turbine blades with ribs was studied numerically [71C]. Internal twisted-tape elements were used to enhance the performance of highly subcooled water in smooth pipes [66C]. Subcritical and supercritical flows in periodic 2-D corrugated channels was studied numerically using the spectral method [61C]. A ribbed coolant passage experiencing a 180° turn was

studied experimentally [56C]. The heat transfer and pressure loss characteristics in turbulent channel flows with surface roughnesses was presented [63C]; a channel with a square bar detached from the wall was also examined numerically [78C].

4.5. Ducts with periodic and unsteady motion

Transient heat transfer measurements were made in an unsteady turbulent and relaminarizing pipe flow [81C]. A single-channel modeling approach was taken to examine the warm up characteristics of an automotive catalyst substrate subjected to pulsatile flow [83C]. The problem of unsteady laminar flow and heat transfer of a particulate suspension in an electrically conducting fluid was studied in the presence of a uniform transverse magnetic field [84C]. The zero-mean oscillatory flow in short channels was examined; the results differ from those in long ducts [87C]. Bundles of circular, triangular, square and hexagonal pipes were subjected to pulsatile flow; longitudinal heat transfer was investigated [86C]. A low Reynolds number k - ϵ model was used to incorporate the role of turbulence on oscillating pipe flow [88C]. A theoretical study was undertaken of the periodic laminar flow developing between parallel plates [85C]. Sinusoidally varying wall heat flux was imposed on laminar flow in a circular duct [82C].

4.6. Multiphase and non-Newtonian flows in channels

An Eulerian–Lagrangian numerical scheme is used to examine the wall heat transfer in a gas–solid particle flow [91C]. A mathematical model was also developed to study the influence of heat transfer and friction between a dilute gas–particle flow and a constant area lance [93C]. One paper considered the drag reduction characteristics and heat transfer of a water suspension flow mixed with fine fibers in a circular pipe [94C]. An electro-resistance sensor and infrared imaging was used to obtain the heat transfer coefficient between a solid–liquid mixture and a circular pipe [98C]. Turbulent gas–liquid flow in vertical pipes was studied to obtain a robust heat transfer correlation [95C]; the forced-convection heat transfer to phase change material slurries was also studied in circular ducts [89C]. An experimental study of mixed convection in vertical annular ducts was conducted for power-law fluids [90C]. The viscoelastic fluid obeying the Phan-Thien–Tanner constitutive equations was studied for laminar pipe and plane channel flow [97C]. The non-Newtonian two-phase flow in conventional and helical-holding tubes was undertaken using a finite-difference approach [99C]. A combined experimental and numerical study examined the laminar mixed convection in a horizontal annular duct for thermo-dependent non-Newtonian fluids [96C]. The behavior of a Bingham non-Newtonian fluid was in-

vestigated for laminar flow conditions through a sudden expansion pipe flow [92C].

5. Separated flows

The majority of papers in the archival literature addressing flow separation and heat transfer focused on bluff body geometries. The fluid flow and heat transfer were examined around a cylindrical protuberance to model the situation encountered when oil tanks are stored in cold environments [25D]. The vortex shedding behind bluff bodies can be stabilized by heating the cylinder in air; heating in water creates an unstable situation [11D]. A Lagrangian–Eulerian description was used to examine the heat transfer changes created by a body moving in the same direction as a fluid in a channel [3D]. The role of struts on the performance of a diffuser was studied experimentally [26D]. The heat transfer characteristics for flow over a tube bank was calculated for laminar and turbulent conditions [27D]. A numerical approach was used to study the turbulent flow past an array of blunt plates; a modified k – ϵ model is used with preferential dissipation [28D]. The complex flow and heat transfer were examined experimentally in flow past two and three cylinders placed side-by-side [30D]. The inverse problem of laminar flow past a heat cylinder was addressed using a finite difference method [12D]. Non-Newtonian flow past an electrically heated cylinder and the associated heat transfer was measured [18D]. An experimental study was undertaken of the pulsatile flow past a heated cylinder; the effect of Strouhal number was documented [9D]. Buoyancy-assisted and opposed flow past isolated and tandem circular cylinders was simulated using a velocity correction method [17D]; unsteady laminar flow past a single and tandem pair of square cylinders was also studied in a channel [21D]. The high-speed flow over a spiked body was examined [14D]; peak heating for the purpose of reattachment was also simulated [15D]. Viscous and thermal contributions to entropy generation were investigated for steady 2-D flow past a parabolic cylinder [4D,5D]. Experiments examined the angle dependence on the heat transfer coefficient for a circular 180° bend in cross-flow [2D]. A low Reynolds number turbulence model was applied to the separation and reattachment phenomena [20D]. Constant wall temperature and constant wall heat flux are imposed on a separation bubble created by mass injection on the opposing wall; DNS calculations are used to examine the flow [24D]. A numerical study was also undertaken to document the turbulent heat transfer of hot flow over a sudden expansion with base mass injection [29D]. A numerical approach was used to investigate the turbulent separated flow and reattachment by local forcing [19D]. Flow past heated curved surfaces having convex and concave shapes was examined under

mixed convection conditions [16D]. The maximum heat transfer rate was increased when supersonic channel-airfoils were employed [22D]. A 2-D finite difference model accurately captured the observed temperature histories of an injection molding process with conformal cooling channels [23D]. Heat transfer is computed and compared to experiment for the crossing- shock-wave/turbulent-boundary-layer interaction [10D]. The mixed convection over a backward-facing step was simulated in three dimensions; both adiabatic and constant heat flux conditions were considered [7D,8D]. The instantaneous heat transfer occurring during compression and expansion in a piston-cylinder geometry is addressed in a numerical study [1D]. Flow and heat transfer past a seven-rod horizontal tube bundle is reported [6D]. A computation study of the heat transfer over a spiked blunt body at Mach 6.8 was presented [13D].

6. Porous media

6.1. Synopsis/Highlights

Heat and mass transfer in porous media was the focus of a great deal of applied and fundamental research. Basic studies of the effective thermophysical properties of a fluid-saturated matrix, fundamental questions on the formation of the governing equations, and the effects of a deformable matrix all received attention. Imbedded surface problems have begun to be treated via conjugate formulations. Packed and fluidized beds remain a challenging technology from the viewpoint of prediction and control of flow fields and transport, and a good deal of modeling and experimental work is underway worldwide. Applied areas that appeared as local activities of porous media research included porous gas-phase and catalytic burners, membrane pumping, cryogenic liquefaction systems, drying of organic materials, assessing growth of forest fires, and geothermal energy production.

6.2. Fundamental advances

Several fundamental advances have appeared in the expanding literature on transport in porous media. At the level of review and codification, a major review of non-aqueous liquid dissolution in porous media was published; it summarizes areas where understanding of fundamentals is strong and where additional experiments and analysis are needed [7DP]. Fundamental work on two-phase flows has resulted in criteria for micro-scale equilibrium [4DP] and the development of conditions for mass and energy jumps at a vapor–liquid boundary within a porous medium [5DP]. Similarity solutions for laminar boundary layer flow of a micro-polar fluid were obtained for a wide range of permeability [15DP].

Entropy generation in natural convection in a porous enclosure was analyzed numerically [1DP] and in an annular packed bed [2DP]. A 1-D model for thermal dispersion was developed from volume averages and multiple scale expansions [11DP]. A macroscopic description of turbulent flow via a two-equation model was developed and shows the need for higher order closure schemes, much the same as for single phase turbulent flow [3DP].

For particulate flows in which the suspended solid comprises nano-particles, the altered mechanism of heat transfer and a prediction of bulk transport properties have been investigated [16DP]. The primary result is that a nano-fluid behaves more like a fluid than a fluid–solid mixture.

Fundamental research concerning coupled heat and mass transfer has addressed the effect of moisture content on transport properties [10DP], molecular level models of hydration and mechanical deformation, [12DP], and saturated versus unsaturated system effects on macro-deformation [13DP]. The effect of mass diffusion in a spherical micro-porous particle was analytically determined, and three limiting regimes of transport were determined [14DP]. Mass transfer in capillary porous bodies was considered via surface and volume-averaged potentials for concentration, heat and filtration [8DP]. Experimental data obtained in rock salt was presented that determine the permeability, the binary diffusion coefficient and the Knudsen coefficients [6DP]. A generalized theory of dependent variable transformation of dispersive transport was developed and extended to include heterogeneous systems with diffusive transport between the fracture and matrix phases and thus develop solutions for the medium overall that conform to conditions encountered experimentally [9DP].

6.3. Property determination

The prediction of the effective stagnant properties and radiative transport within a porous medium continued to be major areas of focus of research. Modeling efforts were largely directed at predicting effective thermal conductivity based on the geometry and packing parameters of the matrix, including contact area [17DP, 23DP, 29DP], thermal constriction resistance at the matrix level [25DP, 26DP], large solid–fluid conductivity ratio [27DP], and the orientation of a fibrous solid phase [20DP]. Two studies included models of effective permeability and thermal conductivity in the computation of overall heat transfer in free and forced convection [22DP, 24DP]. For combined conduction and radiative transport, model studies involved computation of the phonon scattering [21DP] and pore-network simulations [18DP].

Measurements of overall thermal conductivity of compressed graphite and silica gel powder were reported

over a range of preparation parameters and mean temperatures [19DP]. A transient measurement technique was used to determine the effective thermal conductivity of red pine sapwood for several degrees of saturation as function of direction and temperature [28DP].

6.4. External flow and heat transfer

Evaporative heat transfer from a partially saturated porous surface was simulated and measured with a liquid 2-D meniscus attaching two adjacent cylinders [37DP]. Models of several types of porous silicon were used in assessing heat transfer in integrated sensors [45DP]. A general formulation was presented for convection in a double porosity deformable material under the assumption of local thermal equilibrium [41DP]. The variation of permeability and porosity on free convection from a vertical solid surface was shown to produce greater effects on the local heat transfer coefficient near the leading edge where the thermal boundary layer is thin [51DP].

Heat and mass transfer under the influence of non-zero velocity and time-dependent thermal boundary conditions were determined for a continuously moving plate imbedded in a non-Darcian medium [32DP], oscillatory fluid motion past a visco-elastic boundary [48DP], and time-dependent surface temperatures in free convection from a vertical plate [34DP, 42DP]. Heat and mass transfer coefficients in a simple free convection transient on vertical plate was found to depend strongly on heat capacity and porosity ratios [31DP].

Steady free convection from a vertical surface was predicted via a local non-equilibrium model was shown to produce two asymptotic regions near the leading edge that disappear down stream where thermal equilibrium is approached [52DP]. Asymptotic and numerical solutions for the steady buoyant boundary layer and heat transfer above a heated horizontal plate were obtained for fixed and conjugated thermal boundary conditions [39DP]. Free convection from an imbedded inclined permeable plate was computed for a range of wall mass flux and porosity and conductivity variation in the medium [49DP]. Predicted locations of the onset of vortex instability on an inclined imbedded, impermeable plate compared well with measurements and new heat and mass transfer correlations were presented [38DP]. Heat and mass transfer predictions from a wavy imbedded cone were also reported [30DP]. Measurements of mass transfer in natural convection showed that a Brinkman–Darcy flow model is the best predictor of overall mass transfer coefficients when the medium comprises a bed of packed spheres [50DP].

Mixed convection on an imbedded vertical wall was computed for the full range of Peclet, Rayleigh and Gebhart numbers include the effects of viscous dissipation [53DP], surface mass transfer [35DP], a non-iso-

thermal wall [40DP]. The effect of variable surface heat flux and variable permeability for wedge flows were also reported [33DP,36DP].

Conjugated free convection on a vertical thin-walled cylinder and a fin surface was predicted via non-similarity and numerical methods [46DP,47DP]. The combined effects of thermal dispersion and thermal radiation on non-Darcy free convection on a vertical plate were determined using the Rosseland and an ad hoc representation of total diffusivity [44DP]. Laminar, hydro-magnetic heat and mass transfer in free convection over a vertical cone in a uniform porous medium were predicted via non-similarity methods [43DP].

6.5. Packed beds

The analysis of flow and heat transfer in partially filled channels was reported for Couette flow in which the fixed surface bounds the porous matrix [67DP], and the effect of thermal dispersion on forced convection in a partly filled circular duct was predicted numerically via the Darcy–Brinkman–Forchheimer model [68DP,89DP]. A heat transfer model for enhancing forced convection via a porous substrate in the entrance region was shown to produce an optimum in the enhanced Nusselt number based on the depth of the porous layer [63DP]. The design of a porous heat flux sensor was described wherein fluid flows through the sensor to produce a measure of convective heat flux [73DP]. Numerical solutions were developed for porous inserts in otherwise forced flow in a channel [91DP].

Heat transport in fully packed beds was modeled via a quasi-homogeneous model for the laterally uneven distributions of porosity, fluid velocity and effective thermal conductivity, and a comparison with existing measurements suggested that such a model works well for coupled heat and mass transfer [86DP]. Overall effective bed properties were the focus of two related studies [59DP,60DP], and another treated the chemical reaction as a disturbance in the overall energy balance [61DP]. Stochastic methods were applied to describe interparticle heat transfer in a fixed bed [76DP]. A re-evaluation of existing data on temperature and concentration profiles without chemical reaction led to new set of model coefficients [87DP]. Some new results were reported on non-Darcy mixed convection in vertical channel flow [55DP] and in a horizontal channel with a cavity in the lower wall [70DP].

Heat transfer and thermal dispersion in thermally developing forced convection in a sintered metal matrix in channel flow were analyzed, and Nusselt numbers in terms of Peclet number and the thermal conductivity ratio were reported [64DP]. The effects of solids loading on bed porosity and gas flux distribution were determined via analysis of transient temperature response [74DP]. Heat transfer in oscillating channel flow of a

viscous compressible fluid was analyzed via capillary tube and resonance models [71DP]. Volume averaging techniques and a numerical solution of the closure problem were used to establish a volumetric heat transfer coefficient, and results were applied to large Peclet number channel flow [92DP].

Packed beds with inserts designed to improve heat transfer were analyzed for 2-D flow and heat transfer and a range of geometrical parameters pertaining to the inserts [77DP]. Statistical analysis of experimental data on heat transfer in a bed of glass spheres with air as the working fluid established the effects of a variation of inlet conditions on the effective thermal conductivity and the wall heat transfer coefficient [85DP]. Measurements on channel flow containing a pin–fin matrix were analyzed with overall matrix porosity as a factor, and the protrusion of the pin fins through the viscous sub-layer was found to be a major factor in determining heat transfer coefficients and friction factors [90DP]. Measurements of laminar free convection in an open-ended vertical rod bundle was compared to and analyzed via a porous medium approximation, and several key geometrical parameters were identified [62DP]. A multiple ray tracing scheme for the computation on radiative transfer in a packed bed was developed and shown to be computationally faster than probabilistic methods [88DP].

Experiments were reported for a packed bed in both single- and two-phase flow with the aim being to determine the influence of coalescence, inhibition, and effective thermal conductivity on heat transfer coefficients [57DP]. Flow and heat transfer for immiscible conducting and heat generating fluids in a vertical packed channel was analyzed to determine the influence of fluid properties and physical parameters [54DP]. Two-phase turbulent flow through a porous plug was analyzed using a standard k – ϵ model, existing interphase friction coefficients and a turbulent dispersion Prandtl number; a favorable comparison with mean flow data was reported [56DP]. Volume-averaged transport equations were applied to data on gas–liquid counter-current flow with good agreement when model parameters were estimated by extending the model of saturated single-phase flow [69DP]. Correlations for phase holdup in concurrent gas liquid flows were developed from existing data via a drift-flux model with velocity slip [66DP]. Wall channeling in a moving bed was found to decrease gas-to-solid heat transfer coefficients by an order of magnitude below those given by correlations for fixed beds [58DP].

Velocity and temperature distributions in large porosity channel flow showed that outlet flows were nearly homogeneous even though the inlet velocity profile was nearly parabolic over the inlet area [81DP]. Analysis of the effects of heterogeneity in the porous matrix indicated that the effect of a variation of thermal conductivity introduces two opposing effects and thus

makes the Nusselt number a non-monotonic function of the conductivity variation [78DP].

Details of the flow field and fluidization regimes in a fluidized bed were determined by frequency and state-space analysis of pressure measurements in a circulating bed [65DP]. Quantitative flow visualization and determination of the void fraction in a fluidized bed were obtained via neutron radiography [82DP]. Cold flow studies were also carried out via laser phase Doppler anemometry to measure mean and fluctuating velocity, as well as the solids concentration and diameter [75DP]. A limiting case model was developed to determine the drag on falling particle clusters that are observed near the walls of fluid beds [79DP], and experiments were reported on measurements of instantaneous local solids concentration that yielded the parametric effects of particle size and superficial gas velocity on descriptors of particle clusters [84DP]. Numerical predictions of heat transfer in dense gas–solid bubbling fluid beds were carried out via a kinetic theory of granular flow that takes into account particle interactions [83DP].

The effect of bed diameter on near-wall flow bed was determined by measurements of the wall coverage due to clusters of particles in two laboratory scale beds [80DP]. Measurement of suspension-to-membrane wall heat transfer in a circulating bed was deduced from experiments and 1-D fin type models for the exposed surfaces [72DP].

6.6. Porous layers and enclosures

Fundamental work continued on solution methods for steady and transient natural convection in a variety of systems. The lower order Lorenz equations applied to a bottom-heated layer were solved via a decomposition method that yields convergent power series solutions that are applicable to a wide class of problems [116DP]. Non-Darcy, convection in an anisotropic medium was computed via a semi-implicit Galerkin procedure [109DP]. Analytical solutions for free convection in porous layers, along with solutions for several channel and rotating flows, were presented [94DP]. It was demonstrated that convective instability in inclined saturated layers exists at a critical Rayleigh number of zero when an adverse temperature gradient exists parallel to the plates [95DP]. A dual-reciprocity boundary element method for the solution of 2-D cavity flow and heat transfer [110DP].

Steady natural convection in porous cavities was determined for a variety of 2- and 3-D flows: in superposed fluid and porous layers [100DP,102DP], in Marangoni convection in power-law fluids [108DP], in hydromagnetic convection in tilted enclosures [103DP], and in open ended cylinders with spatially varying heat flux boundary conditions [98DP]. Cavity flow and heat transfer were determined numerically when one of the

vertical walls is wavy [105DP]. The case of an arbitrary non-rectangular cavity was treated with a body fitted coordinate transformation [112DP], and the problem of flow and heat transfer between concentric elliptical cylinders was solved numerically [107DP]. An interesting study of a cavity filled with capsules containing phase-change material in a rigid matrix demonstrated that a maximum capsule density exists that limits disperse diffusion over the entire system [104DP].

Transient natural convection inside porous cavities was determined via hybrid numerical and analytical methods employed integral transforms so as to produce a system of coupled, nonlinear ordinary differential equations [96DP]. Three-dimensional fluctuating flow and heat transfer with variable permeability and a transpired boundary exhibits a reduction of velocity amplitudes with an increase of permeability or the frequency of permeability variation in the matrix [113DP]. A Nusselt number correlation for lid-driven cavity flows with a vertical temperature gradient were determined numerically for laminar convection [93DP].

Double diffusive convection induced by horizontal gradients of temperature and concentration exhibited two types of solutions at steady state according to whether the heat and mass gradients were aiding or opposing [97DP]. In slender anisotropic enclosures, analytical solutions are shown to exist for aspect ratios greater than three and to exhibit great sensitivity to parameters that characterize anisotropy [99DP]. The onset of double-diffusive convection in a rectangular cavity was shown to depend on the aspect ratio of the cavity and to exhibit a supercritical Rayleigh number and an over stability [106DP]. Finite frequency modulation of double-diffusive convection in a square cavity was demonstrated via linear harmonic oscillations in the vertical direction [114DP].

The filling of fiber reinforced molds was predicted numerically based on mixed Eulerian–Lagrangian approach under a two-temperature model [101DP]. A related study for a non-reactive fluid shows analytically and experimentally that boundary effects are important for Reynolds numbers on the order of unity or greater; below this value, Darcy flow is applicable, and boundary effects are not important [118DP].

Geophysical heat transfer problems were modeled in the context of porous-cavity heat transfer. The onset of free convection in fracture zones was modeled to test prior work that indicated that critical Rayleigh number greatly exceeded that for the horizontal layer [115DP]. The development of layered structures due to magma intrusions in the evolution of the Earth's mantle was numerically simulated as a transient double-diffusive problem in an initially stable layer; when a density interface develops that is strong enough to arrest ascending plumes, the layering process ends [111DP]. A 2-D steady solution for buoyant flows induced from a nuclear waste

repository in unfractured and fractured crystalline rock demonstrated that fluid discharge at the boundary is a possibility in the fracture flow case [117DP].

6.7. Coupled heat and mass transfer

Several analytical solutions for coupled heat and mass transfer have appeared for systems of general applicability. Similarity and non-similarity solutions were obtained for a cone imbedded in a porous medium [133DP,177DP], magneto-natural convection in Hiemenz flow [132DP], mixed magneto-convection from a vertical plate in a porous medium [130DP], hydromagnetic mixed convection with a temperature-dependent heat source on a flat plate with suction/injection [128DP], and hydromagnetic convection from imbedded permeable surfaces [129DP,131DP]. Laplace transforms and a subsequent transform function were used to reduce the coupled heat and mass transfer problem to a single fourth order, ordinary differential equation [134DP]. Nusselt numbers on a buried cable in either dry or saturated soil were determined from the numerical solution of the governing equations [124DP]. The interface between and non-wetting phases in the absence of mass transfer for 3-D porous materials was determined via an image analysis, which was shown to be superior to the use of percolation networks [160DP].

Experimental data were presented for enhanced condensation on a fluted tube surface with a thin porous coating [175DP]. Heat and moisture transfer with sorption and condensation in clothing assemblies were determined via a dynamic numerical model that takes into account the effect of water content on the effective thermal conductivity [147DP]. Permeability effects on condensation heat transfer coefficients, film thickness and velocity profiles were determined for a vertical plate imbedded in a porous medium via a Brinkman–Darcy formulation that included local macroscopic inertia [163DP].

A review of the role of fire and heating on water repellency in soil includes effects of vaporization and soil chemistry, such as occur in wildland environments [139DP]. Gas phase growth via pressure reduction in 2-D porous media was successfully modeled using an etched micro-network and an analysis taking into account supersaturation, wettability and gravity [144DP]. Liquefaction of cryogenic gases in a two-stage magnetic particle bed refrigerator was modeled to determine the effects of key parameter and the optimal operating point [178DP].

A numerical model of heat and mass transfer in turbulent channel flow over a saturated hygroscopic porous layer shows that moisture migration takes place from the warm interior to the relatively cool periphery [167DP]. Transient drying of a metal hydride bed was analyzed numerically taking into account the kinetics,

the significance of assuming local thermal equilibrium, and the neglect of convective energy transport [164DP]. An analysis of moisture transport driven by thermal gradients in a porous membrane was reported with application to membrane-based humidity pumps [179DP].

Combined thawing and mass transfer at 0 °C, such as occurs in cold immersion storage, was found to exhibit a sharp thawing front that separates a frozen inner layer from a thawed non-impregnated outer layer [158DP]. Experiments to simulate coupled heat and mass transfer at the product–freezant interface showed that a non-frozen surface layer forms in the product and that thawing follows a classical diffusion timescale [157DP].

A variety of drying processes in wood and foodstuffs received analytical and experimental attention. Vacuum-contact drying was analyzed using the water potential formulation [141DP]. A new experimental method for determining heat/mass transfer coefficients was developed by indirect measurement of the water potential over time [173DP]. A multi-component, multi-temperature model for forced convective drying was developed using data from the various drying regime [140DP]. A phenomenological, 2-D multi-component model was developed where capillarity, bulk diffusion and diffusion of bound water due to the gradient of the chemical potential are the simultaneous transport mechanisms [172DP]. A finite-volume finite time-domain algorithm to solve Maxwell's equations was developed to determine the steady state power distribution in micro-wave heating of wood with low moisture content [182DP]. A 1-D analysis was of high-temperature drying of softwoods, where the permeability is relatively large and moisture transport occurs in the fibers and in bulk form, was presented and favorably compared to measured moisture content profiles [165DP]. Batch fluid bed drying for apples was analyzed to reveal the importance of internal heat transfer and state of the gas along the height of the bed [174DP].

Combustion of a moving gas in a semi-infinite porous medium was analyzed to determine the effects of heat transfer to the matrix and the conditions under which combustion does not take place at the external surface [125DP]. Experiments and numerical were also reported on the low- to high-velocity regimes of gas-phase and catalyzed combustion in such a system [126DP,143DP,145DP,161DP]. Thermal radiation and the transparency of the matrix were shown to have measurable effects on combustion efficiency and the matrix temperature [184DP]. Experiments on flammability limits for hydrocarbon–air mixtures show that matrix geometry, matrix heat transfer and flow effects must be taken into account to predict flammability data and in modeling extinction mechanisms [142DP]. Numerical analysis and experiments on 2-D porous burners for premixed methane–air combustion produced similar results with good agreement with experiments [123DP].

Transient heat and mass transfer in a reacting packed bed was shown to have oxidant-limited and reaction-limited modes, which were verified experimentally [170DP]. Experiments on bulk phase water vapor diffusion in a silica gel packed bed were reported [176DP]. Packed beds for methanol steam reforming were compared to a novel use of a coated heat exchanger to improve conversion efficiency and transient operation [138DP]. Variations in overall reaction kinetics in a catalytic packed bed were attributed to interparticle heat transfer [171DP]. A convection–dispersion model and an effective thermal diffusivity were used to describe the variation in solids temperature in a reacting packed bed [135DP], and a 1-D model successfully modeled combustion of char particles in an overfed packed bed [137DP]. Experiments on overall mass transfer in an absorbing bed using an insert to prevent solution carry over was reported [136DP].

Fluidization regimes in packed bed via injection of carbon dioxide were experimentally mapped for a sub-critical to super-critical conditions [162DP]. A transverse magnetic field was used to alter the heat transfer and flow in a fluidized bed of ferro-magnetic particles [119DP]. Circulating fluid-beds with and without reaction were the focus of analytical and experimental studies aimed at species concentrations, temperature profiles and local velocities [120DP–122DP, 152DP, 156DP, 168DP, 169DP]. Measurements were reported of heat transfer coefficients on an immersed surface in a gas–solid fluid bed [159DP]. Particle tracking was used to determine overall bed properties in a transient reacting gas–solid bed [149DP].

Structural change of the porous medium due to reaction, such a might take place in forest fires and pyrolysis in packed beds, was the objective of both numerical and analytical work [146DP, 148DP, 153DP, 154DP]. Double-diffusive convection in a deformable, saturated medium with temperature-dependent reaction was computed using a fully couple model for temperature, species, and pore flow [181DP]. Sintering of the porous medium with reaction as shown to be sensitive to heat transfer at the flame front [155DP]. The equations governing the physico-chemical convective dynamics of heterogeneous gas–solid reactions were reviewed with respect to pore obstruction [166DP] and the material synthesis [127DP].

Geophysical heat and mass transfer where the host rock is present were the subject of several theoretical and experimental studies. Layered hydrothermal systems with upward through flow and mineralization were numerically investigated to determine the most probable precipitation regions [180DP]. Fractured hydrothermal systems that have suddenly dilated were analyzed to determine heat transfer and fluid withdraw from an initial state close to vapor saturation [150DP]. A negative feedback between flow and heat transfer was shown

to exist in large-scale density-driven circulation in structures of the type seen in marine carbonate platforms [151DP]. Buoyancy driven flow with phase change in a symmetrically heated vertical channel was analyzed to include capillary effects [183DP].

7. Experimental methods

Experimental methods play a key role in heat transfer studies, not only in fundamental research, but also in a number of important applications and engineering systems including energy conversion, transportation, heat exchangers, and many others. Valid and accurate data are required to improve classical heat transfer techniques, as well as in the development of new and important methods. Although, some measurement techniques and systems are included in other sections of this review where they are used in specific applications, the present section considers developments of a more general nature.

7.1. Heat flux measurement

An overview [6E] describes the National Institute of the Standards and Technology high-temperature black bodies used in calibration of heat flux sensors. A heat flux gage using a sputtered thin film thermometer on one side of an insulating layer and a thermocouple in a metal arm on the other side has been developed [8E] for studying rapid fluctuations in heat transfer. Corrections have been applied in the use of button gages that determine heat transfer to a metal wall suddenly exposed to a hot flow [5E]. A “sandwich hologram” can determine the heat transfer coefficient in transparent fluids [10E]. Heat transfer measurement techniques have been developed for solidification problems [7E] thermodynamic and kinetics analysis [2E] heat transport between the atmosphere and an ocean surface [4E] fluid-to-particle heat transfer [9E] non-intrusive studies of a dense suspension of gas and fine solids [3E] and use in pulsed excimer laser calorimeters [1E].

7.2. Temperature measurement

A number of techniques have been reported for measuring temperature. Some of these are optical and can be non-intrusive in nature. Other reports have presented improvements of widely used systems such as liquid crystal temperature measurement. Rayleigh scattering has been used to measure temperatures in air [25E]. Laser-induced fluorescence was used for temperature measurement in a model combustor [17E] and in the flow field in a high-enthalpy arc jet facility [11E]. Other optical techniques include nuclear magnetic resonance spectroscopy to monitor electrolyte tempera-

ture in capillary electrophoresis [14E] and laser-based thermo-reflectance to measure temperature at a transparent solid–liquid interface [12E]. Particle image velocimetry techniques have been used in combination with a shadowgraph to measure temperature in a reacting flow [18E]. Reviews describe applications of infrared thermography in gas turbine film cooling measurements [23E] and calibration techniques for liquid crystal temperature measurement [15E,21E]. Systematic errors in temperature measurement due to presence of a temperature sensor have been described [20E]. Techniques presented for temperature measurement include a differential scanning calorimeter [22E], metaloxide fibers for calibration of high-temperature gas measurements [13E], algorithms for use in passive thermo-acoustic tomography [19E], a system to determine wafer temperature during integrated circuit processing [24E] and gallium arsenide crystals for temperature measurement in low-pressure plasmas [16E].

7.3. Velocity and flow measurements

Calibration systems have been developed for hot wire anemometers at low flow velocity [27E]. Ultrasound scattering has been used to study the transition to turbulence in a thermal plume [26E]. Other reports describe the use of liquid crystals for measuring both heat transfer and surface shear stress [28E], combined particle image velocimeter (PIV) and planar laser-induced fluorescence for studying turbulent mass transport mixing [29E], and a thermal system for measuring water flow in soil [30E].

7.4. Miscellaneous measurements techniques

Recent probe developments include a double sensor probe [32E] to determine local interfacial variables in two-phase gas–liquid bubbly flows, and a four-sensor conductivity probe for time average local two-phase flow measurement [34E]. Techniques were developed to measure thermal conductivity of re-melted volcanic rock materials [31E] and thermal diffusivity at room temperature using laser pulsed heating [36E]. An inverse solution method for estimating both thermal conductivity and contact resistance in heat transfer systems [33E] has been described. A two-wire in-core instrument can measure energy deposition in a nuclear reactor [35E], and a laser focus displacement meter has been developed and applied to measure waves flowing on films in vertical tubes [38E] and on flat vertical walls [37E].

8. Natural convection-internal flows

8.1. Fundamental studies

One of the classical issues in the Rayleigh–Benard (R–B) problem, the relationship between Nusselt num-

ber and Rayleigh number, has been addressed by considering the effect of the flow Reynolds number [1F]. A unifying theory is presented in which the heat transfer is correlated with the $Ra Pr$ product over a wide range of Rayleigh number.

8.2. Heat generating fluids

The onset of thermal convection caused by microwave heating in a bounded vertical cylinder was predicted using linear stability analysis [5F]. Results of convection of liquid in a square enclosure [3F] and of liquid metal in a rectangular enclosure [2F] were presented. More practical investigations include the simulation of convection in a microwave cavity [6F] and measurements in a hemispherical cavity [4F] that simulates a nuclear reactor lower head geometry.

8.3. Thermocapillary flows

Rayleigh–Benard–Marangoni convection continues to receive interest. Tomita and Abe [14F] have shown that hexagonal convection occurs when the surface tension effect is stronger than the buoyancy effect. A type of mixed roll and hexagonal convection is found when both effects are of comparable magnitude. Flow of liquid metal in a square cavity with a uniform vertical magnetic field was investigated [11F]. A novel numerical method based on the stream function – vorticity formulation was used to simulate flows in a rectangular cavity with a free surface [8F]. Oscillatory Marangoni flow in liquid bridges was reported by Lappa et al. [10F].

Studies of Marangoni convection within electrostatically levitated droplets have been reported [12F,13F]. Results show that the combined effects of surface tension and the electromagnetic field cause the drop to deform into an ellipsoidal shape. Balasubramaniam [7F] analyzed the motion of a spherical drop within a uniform temperature gradient when the Marangoni number is large. A theoretical study was presented in which the flow of liquid that has been sprayed onto a moving fiber was simulated [9F].

8.4. Enclosure heat transfer

Heat transfer in a vertical square or rectangular cavities continues to receive considerable interest with most of the work being numerical rather than experimental. Several different combinations of thermal boundary conditions and flow properties have been studied. Secondary flows [32F] and optimum thickness for window applications [16F] were reported for cavities with high-aspect ratio. Ishihara et al. [27F] considered localized heat sources on one vertical wall and Leal et al. [33F] included variable fluid density in the body force term. Numerical simulations were conducted on the

classical geometry with opposed heated and cooled vertical walls using a pseudo-spectral Chebyshev algorithm [46F]. Finite element solutions compared favorably with the benchmark results published by de Vahl Davis [29F]. Experimental work on the flow and heat transfer in a vertical air filled cavity was conducted by Tian and co-workers [44F,45F] and Betts and Bokhari [18F]. A 1-D turbulence model was shown to reproduce available direct numerical simulation results for natural convection in a vertical rectangular slot [23F]. Aydin and Yang [17F] simulated the heat transfer in a cavity with localized heating on the bottom surface and cooling from both sides. Two numerical studies were presented in which the fluid had a density maximum such as water near 4 °C [28F,34F].

Rayleigh–Benard convection in horizontal layers has been studied using a RANS model [30F] to investigate transient effects. The route to chaos in a fluid layer was studied using a Galerkin representation of the governing equations [47F]. Experiments using water reached a Rayleigh number of 2×10^{10} [43F] and tests using cryogenic helium gas attained a Rayleigh number of 2×10^{15} [38F], considered to be the highest ever achieved in a controlled laboratory setting. Sezai considered the effects of different thermal boundary conditions, heated from a patch on the bottom [39F] and cooled from the sides in addition to the top surface [40F]. The heat transfer was reported to have increased by more than 76% when the upper and lower surfaces were roughened [24F]. Numerical simulations were performed to study the effect of strongly temperature-dependent viscosity [22F] and an electrochemical technique was used to develop a correlation between the Sherwood number and the thermal and solutal Rayleigh numbers [31F].

Double-diffusive natural convection was investigated numerically in a cavity with conductive and diffusive walls [26F] and in a square cavity in the neighborhood of the maximum density of the fluid [42F]. Siginer and Valenzuela-Rendon [41F] studied the flow and instability of natural convection in an inclined slot containing a grade fluid. Numerical studies of flow in a vertical cylinder heated from below [20F,37F] and having azimuthally varying wall temperature [21F] were presented. Investigations of contained bodies includes the study of heat transfer in a conducting cubic heat-generating body centered within a larger cubic enclosure [25F]. Natural convection in pitched roof attic spaces has been simulated [15F,36F]. A numerical analysis of heat transfer through a shallow rectangular cavity was presented [19F] and a parametric study of heat loss from heat sources placed into an enclosure was reported [35F].

8.5. Vertical ducts and annuli

Experimental results and numerical solutions were presented for heat transfer from a heated tube centered

between two vertical walls of lower temperature [49F]. The heat transfer decreased then increased unexpectedly as the Rayleigh number increased. Heat transfer in a vertical concentric cylindrical annulus with radial temperature gradient was studied by Bahloul et al. [48F].

8.6. Horizontal cylinders and annuli

Thermal and hydrodynamic instabilities were reported in air-filled annuli of small aspect ratio [50F].

The effect of eccentricity on the heat transfer in a horizontal annulus was studied by Yeh and Chang [51F,52F] where the annulus opens into a larger cavity.

8.7. Mixed convection

The majority of publications in the area of mixed convection considered flow through channels and pipes. Numerical [65F] and experimental [66F] investigations were made of mixed convection in a fluid injected between two horizontal circular plates. Flow in a low aspect ratio channel was studied to predict the behavior caused by small accelerations encountered in spacecraft [63F]. The effect of mixed convection on visco-elastic fluids in a horizontal pipe was reported [58F]. Brinkworth [56F] presented a procedure for calculating the flow rate and heat transfer for laminar free and mixed convection in inclined ducts.

Mixed convection in rotating systems were studied by Enger et al. [57F] and Auernhammer and Brand [54F]. A numerical study was conducted on the effects of moving sidewalls on the flow and heat transfer in a cavity heated from below [55F].

Several numerical studies have been conducted on natural convection in a vented cavity with the primary application being the cooling of electronic equipment [53F,59F–61F,64F]. The heat transfer in a marine reactor core subject to rolling was found to be well correlated with the Richardson number for the rolling motion [62F].

8.8. Complex geometries

Several unusual geometries and thermal boundary conditions have been investigated this year. Heat transfer from two vertical plates or a centrally located heating block were studied in a larger 2-D enclosure [67F]. Heat transfer from a conducting block located in a cavity [71F] and between two coaxial square containers inclined by 45° [70F] were investigated. The effects of spacing between vertically mounted heating strips in a vertical cavity [69F] and time varying heated strips placed on the bottom of a horizontal channel [68F] were reported. Yu and Joshi [72F] studied the cooling of partially open horizontal enclosures containing discrete flush mounted heat sources.

8.9. Fires

A fire growth and smoke movement model developed for multi-compartment buildings by the National Research Council of Canada was presented [75F]. Experimental studies include investigation of the effect of ventilation airflow in tunnel fires [77F] and the ignition signatures that describe the onset of self-sustained downward smolder [73F]. Theoretical studies include the influence of flame heat transfer on the flame spread on solid surfaces [74F] and the modeling of confined jet fires using three different combustion models [76F].

8.10. Miscellaneous

Thermal convection models have been developed to explain the differences in geologic histories in various regions of North America [79F]. Free convection has been found to increase the heat flux to semiconductor wafers in CVD reactors [81F]. Measurements of SF₆ during quenching in low gravity environment show a striking observation that the gas temperature exceeds that of the heating walls by a considerable amount [82F]. Two papers report the effect of transport between two liquid layers of different density [78F,80F].

9. Natural convection-external flows

9.1. Vertical plate

Studies of laminar buoyancy-driven convection of heat from a vertical plate include the use of a similarity transformation and heat functions for isothermal or constant heat flux boundary conditions [5FF]. Variations in fluid conditions that were considered include heat transfer to a stratified fluid with time varying boundary conditions [3FF], variable viscosity and thermal diffusivity [6FF] and partly dissociated gases [7FF]. Experiments in water, direct numerical simulation and linear stability analysis were used to study convective instability near a suddenly heated vertical wall [4FF]. Conjugate conduction–natural convection near a thin vertical strip with internal heat generation was investigated [9FF] and the effect of an attached or adjacent square solid element was reported [8FF]. The effects of wall suction, magnetic field and Prandtl number have been studied numerically [10FF] and a series expansion method was used to determine the limiting diffusion current for a thermal perturbation under conditions of simultaneous heat and mass transfer to the vertical electrode [1FF]. Measurements and predictions have been presented for turbulent natural convection adjacent to an isothermal vertical wall containing an adiabatic backward-facing step [2FF].

9.2. Horizontal and inclined plates

Studies of heat transfer above heated horizontal plates include rectangular plates of different aspect ratios [14FF,17FF], the effect of surface roughness [16FF] and mixed thermal boundary conditions in a micro-polar fluid [15FF]. Experiments and numerical solutions were presented for heat transfer from a downward-facing heated plate with rectangular grooves [13FF].

Liquid crystal thermography was used to provide full field measurements of the influence of longitudinal vortices on an inclined heated plate [12FF]. Numerical results were obtained for turbulent flow [18FF] and transient 3-D laminar flow [11FF] over inclined plates.

9.3. Channels

Experimental results were obtained for heat transfer from a vertical plate mounted within a ventilated cabinet [23FF]. Numerical methods were used to study the appropriate boundary conditions to use for a partially open cavity [22FF], the cooling of heated objects mounted in a vertical channel [20FF,21FF] and fin geometry and temperature difference for air cooling of fin arrays [19FF].

9.4. Cylinders

A correlation for predicting the extent of electrohydrodynamic enhancement of natural convection from horizontal cylinders was presented [28FF]. Heat transfer measurements were obtained for natural convection from a vertical array of two horizontal cylinders [24FF] and a finite element method was used to predict the cooling of two open-ended seven-rod bundles of horizontal cylinders [27FF]. Heat transfer from a vertical cylinder with variable surface temperature [26FF] and with combined heat and mass transfer [25FF] were presented.

9.5. Buoyant plumes

Two numerical studies [29FF,32FF] considered plumes in an enclosure such as in a room. Comments regarding the use of experimental balances in the study of thermal plumes were given [33FF]. Theoretical results have been presented for very weak plumes or fountains in large containers [30FF,31FF].

9.6. Mixed convection

Several studies have been reported that consider mixed convection adjacent to a heated vertical flat plate [38FF,39FF,41FF,42FF] or cylinder [44FF]. Measurements have been made on surfaces in a ventilated building [35FF] and in a horizontal converging channel

heated from below [37FF]. Numerical results have been presented for mixed convection in a micro-polar fluid on a horizontal flat plate [40FF] and in a water model of continuous casting tundish [43FF]. Two investigations were conducted on heat transfer from a continuously stretching surface [34FF,36FF].

10. Heat transfer in rotating systems

10.1. Synopsis/highlights

Moderate activity on rotating flows in 2000. Rotating disks yet attract a good deal of attention, with prediction of 3-D flow and heat transfer yielding fundamental advance; rotating disks in a confined geometry occur in many applications and several related studies on heat and mass transfer are reported. Materials processing technologies and geophysical heat transfer motivated research on rotational effects on convective heat transfer in annular systems. Some interesting and important experimental data were reported. The prediction of flow and heat transfer in multi-pass rotating channels continues to receive a good deal of attention, and research is motivated largely by gas turbine blade cooling technology.

10.2. Rotating disks

Fundamental measurements on convection due to normal jet impingement on a rotating disc were obtained using liquid crystals to estimate local temperature differences over a range of rotational speeds and jet Reynolds numbers [6G]. The influence of the Coriolis force on convection on a rotating transitional boundary layer was also experimentally shown to enhance heat transfer coefficients when the forces act toward the wall [1G]. Three-dimensional flow and heat transfer in a stagnation flow CVD reactor was shown to maintain its symmetry with relatively low inlet Reynolds numbers and/or rotation rate of the working surface. [9G]. Similarity solutions for time-dependent heat and mass transfer, with phase change, from a rotating disk were obtained where the angular velocity varies inversely with time [8G].

Rotating disks in ventilated passages, or enclosures, were the subject of experimental and numerical work. Heating by viscous dissipation between two disks, one of which is rotating, was investigated experimentally and shown to be predictable by simple theoretical models [2G]. An extensive numerical study was carried out on a ventilated disk for which inlet Reynolds number, rotational speed, shroud clearance and wall temperature were varied in the determination of Nusselt numbers and skin friction coefficients [5G].

Heat transfer from rotating finned tubes was the subject of experimental study. Measurements of heat transfer coefficients on rotating fins have been obtained using infrared thermography and the relative influences of rotational forced and natural convection have been estimated via correlations [10G]. These same researchers have also reported measurements of flow fields between two fins where a superposed external flow exists [11G]. A novel rotating-disk evaporative cooler with parallel airflow was developed, and bench scale tests coupled with numerical analysis demonstrated higher cooling capacity and greater coefficients of performance [4G]. A numerical study motivated by disk brake cooling reported the influence of convective heat transfer from a rotating solid or heat pipe disk with a superposed parallel airflow [12G]. A related study reports turbulent heat transfer to a disk for both the constant wall temperature and constant wall heat flux boundary conditions [7G], and extensive 3-D numerical work was completed for film-cooling effectiveness for a turbine blade with 172 cooling holes in eight rows [3G].

10.3. Rotating channels

Several aspects of convective heat transfer in rotating channels were investigated largely via numerical means. Strong curvature effects on laminar flow in square and circular ducts were shown to give rise to non-symmetric secondary flows at low Reynolds and Rossby numbers [21G]. Reynolds stress budgets were computed via DNS for a pipe where near-wall regions are altered due to high-rotation rates [20G]. Large eddy simulation models were developed for a channel with transverse rib turbulators [19G]. Relaminarization of turbulent flow in entrance region flows was computed and successfully compared with experiments [17G].

Convection and flow in rotating multi-pass channels was investigated to determine pressure drop and heat transfer characteristics. Heat transfer in a two-pass square channel was shown to be strongly affected by Reynolds stress anisotropy and the 180° flow turn [15G,16G]. Pressure drop in a smooth square channel with a sharp 180° bend was measured and shown to be strongly affected by rotation and less so on Reynolds number [22G]. The combined effects of rotation and skew angle in a two-pass duct were also investigated numerically [14G]. Active control of reversed flow and mixed convection via transpiration in a two-pass duct was analyzed numerically and shown to have different effects for the radial-outward and radial-inward flows [18G].

In somewhat specialized studies, measurements of discharge coefficients on a rotating shaft, such as would exist in a gas turbine, were reported as a function of the rotation of the surface [13G], and the numerical predictions of flow through a helical pipe rotating about the

center of curvature show a sharp peak when rotation is opposite to the pressure-driven flow [23G].

10.4. Enclosures

Three-dimensional natural convection in rotating cylinders was investigated numerically and experimentally for a range of Reynolds and Richardson numbers, as well as rotational parameters, stratification effects, and thermal boundary conditions. A variety of effects of rotation were observed on boundary layer regions [32G], vortical interactions in geophysical flows [27G], and heat transfer coefficients [24G,35G]. Coriolis forces were shown to completely suppress convection in water near the density maximum point [40G]. A similar result was observed for solutal convection in shallow rotating electrochemical cells for certain Schmidt and Ekman numbers [43G].

Rotational effects on buoyant flows encountered in materials processing technologies were investigated numerically for time-dependent high pressure vertical Bridgman growth [44G]. Similar simulations were carried out but with flow induced by rotating magnetic field [42G]. In both studies, fluid rotation was seen to induce mixing and promote secondary flow.

Direct numerical simulation (DNS) of turbulence and compressed swirl flow in a rotating flat cylinder was compared with prior work based on the Reynolds-averaged Navier–Stokes equations, and the latter were shown to reproduce the results of DNS, as well as existing experiments [29G].

Flow and heat transfer in a rotating annulus were investigated numerically and experimentally generally for lateral heating but under different conditions on rotation and internal stratification. Flow in a multi-layered double-diffusive regime under uniform rotation shows that temperature fields develop continuous shapes but that concentration profiles can develop jumps at the Taylor number increases [34G]. Measurements on Couette–Taylor flows using electro-diffusion probes at the walls and internal to the flow indicated the existence of the Ekman vortices at rotation rates smaller than the critical rate for the onset of Taylor vortices [38G]. Centrifugal forced convection in a short annulus containing a Carreau-fluid shows shear thinning effects, higher heat transfer coefficients and the possibility of oscillatory flow [30G].

Analytic and numerical solutions for centrifugal forced flow in a gas-filled annulus were obtained for the free molecule and hydrodynamic limits [25G]. Flow in an eccentric annulus containing a pseudo-plastic fluid and an axial pressure gradient was analyzed to determine axial discharge rate under various rotational rates of the inner cylinder [28G], and both experiments and numerical analysis were reported for a similar system but with a Newtonian fluid [26G].

Measurements of high Rayleigh number thermal convection in a rotating hemispherical shell were reported where centrifugal forces and gravity successfully simulate gravity in the Earth's core; major results include the identification of three major Raleigh regimes of flow, the existence of geostrophic turbulence, and so-called dual convection driven by cold and warm plume flow [39G]. Flow bifurcation and heat transfer at each mode of flow in a spherical gap with an inner rotating surface was numerically predicted for low to moderate Reynolds numbers [36G].

An experimentally validated model for the mixing of solids in a rotating drum was developed based on correlations for mixing rate and material contact [41G]. Mixing of granular materials due to an embedded rotating blade was measured using positron emission tracking to produce maps of the velocity field and hence circulation patterns [33G]. Heat and mass transfer measurements in a centrifugal fluid bed dryer were reported for various superficial gas velocities, particle size, bed thickness and rotational speed [37G].

A model was developed for heat transfer and flow in co-rotating twin screw extruder during the fluid-filling phase, and viscous heating effects on the screw were determined [31G].

10.5. Cylinders, spheres, and bodies of revolution

Similarity solutions for unsteady flow in the stagnation region of a rotating sphere with a magnetic field show that heat transfer increases with acceleration and the magnetic parameter [46G]. Forced convection from steadily rotating and oscillating cylinders were obtained for Newtonian and non-Newtonian fluids [45G,47G].

Flow and heat transfer calculations in a pipe containing a coaxially rotating disk were reported for laminar pipe flow and large disk-to-pipe diameter; rotation is shown to substantially affect the heat transfer rates, primarily by introduction of swirl flow [48G].

11. Combined heat and mass transfer

11.1. Ablation

A number of studies consider the thermal response of ablating materials. Researchers considered the onset of ablation in the hypersonic (Mach 5) flow regime [4H]. The study extended previous investigations by considering the effects of the cavity on ablation onset times using both experimental and computational methods. Picosecond laser ablation was investigated using joint computational/experimental studies [2H,3H]. These studies captured the formation and evolution of the plasma during early stages of the ablation process. Another hybrid experimental/computational investigation

studied crater properties during nanosecond laser ablation of silicon [6H]. In considering the ablation of metal/polymer composite materials, researchers studied the energy transfer between the metal and the polymer which results in the ejection of the metal powder [5H]. Researchers also modeled ablation using an effective inverse Stefan number. The model was used to perform a parametric study of the proposed inverse Stefan model in simulations of 2-D ablation [1H].

11.2. Film cooling

Film cooling is an effective method of heat transfer and very useful in protecting surfaces from the effects of thermal stress. Several studies considered the film cooling of turbine blades. These include use of the heat transfer \tilde{n} mass transfer analogy [14H], and the utilization of multi-disciplinary optimization methods in turbine blade design [21H]. A survey of past accomplishments as well as work which needs to be done was also performed [19H]. Researchers also considered the angle of coolant injection [16H], and the shape of the injection holes [7H,9H,12H]. The effect of the orientation angle on the boundary layer temperature was also considered [13H]. Flow visualization and numerical simulations were utilized in investigating heat transfer in short length-to-diameter injection holes [10H]. Computational studies were used to investigate the effect of flow ratios, hole spacings, and injection angles on secondary vortices and the ensuing heat transfer [18H]. The film cooling of cylindrical [17H] and other convex surfaces were also investigated [8H]; these too considered both cylindrical and shaped holes [15H]. The cooling of films was also investigated. Researchers considered the cooling of a blown film due to the impingement of turbulent air [20H], and the cooling of visco-elastic films during extrusion [11H].

11.3. Jet impingement heat transfer – submerged jets

A number of studies involving the heat transfer in submerged jets (air issuing into air, liquid issuing into liquid) impinging on solid surfaces have been performed. Researchers investigated the heat transfer due to multiple jet impingement by considering the spacing between nozzles, the jet Reynolds number, and the spacing between nozzle exit and the surface of impingement [24H]. Another study considered the shape of the nozzle – from circular to elliptical \tilde{n} in enhancing heat transfer [29H]. Three studies considered the effect of jet inclination on heat transfer [22H,33H,35H]. The effect of jet nozzle contouring was investigated by considering a slot jet impinging on a circular cylinders [30H]. A study of flow pulsation on the characteristics of planar jet impinging on a heated surface was performed [31H]. The enhancement of heat transfer from a discrete heat source using

multiple jet impingement of air in a confined arrangement was investigated [26H]. Researchers studied cooling of alumina disks using a high-velocity air jet [34H]. The effect jet Reynolds number was investigated under a variety of pin-fin heat sinks under air impingement [27H]. Experiments were performed to study slot air jet impinging on a triangular rib-roughened wall [28H]. Additionally, several numerical simulations were performed. Researchers utilized a nonlinear eddy-viscosity model in performing Reynolds-averaged Navier–Stokes simulations of separating and impinging flows [25H]. Surface pressure distributions and streamlines were computed for different impinging jet configurations [32H], and the conjugate heat transfer due to the impingement of a high Prandtl number fluid was studied [23H].

11.4. Jet impingement heat transfer – liquid jets

A jet in which the issuing stream has a density significantly higher than that of the ambient fluid is said to be a liquid jet. Because of their relatively high-thermal conductivity liquid jets are often used for jet impingement heat transfer. The interaction of propagating premixed flames with obstructing bodies was considered [43H]. A water-cooled, cylindrical combustion chamber was used to investigate the effect of injection location and percentage of liquid fuel during gaseous combustion [36H]. The surface temperature of a layer of liquid in the process of combined heat and mass transfer was predicted [41H]. Jets of high Prandtl number fluid impinging on a substrate with heat sources were modeled as a conjugate problem [38H,44H]. Heat transfer measurements were made of jets impinging on a dimpled surface using a transient liquid crystal technique [37H]. Simulations utilizing a volume-of-fluid method were used to study the break-up of liquid jets upon impactation with a liquid pool [45H]. A combined experimental and computational study of a high Schmidt number slot jet was performed [40H]. Gas absorption from a rising gas plug was studied [42H]. It was found that the mass transfer rate decreased when the dimensionless heat of absorption was increased. The effect of nozzle shape on heat transfer enhancement was investigated in a steam-jet refrigeration system [39H].

11.5. Transpiration

Several studies involving transpiration were performed. A simulation model was developed to predict the effects of heating system location on transpiration in a greenhouse crop [48H]. Another study analytically investigated the effect of evaporation from a wetted wall on convective heat transfer [46H]. Researchers considered the effect of thermal properties of lysimeters in measuring the evaporation of water from soil [49H]. The

cooling of ultrasound applicators for interstitial therapy was investigated [47H].

11.6. Drying

Heat and mass transfer are integral to drying. A wide variety of studies utilizing computational methods were performed. These include the drying of foodstuff [51H, 68H, 70H, 75H, 86H], polymer solutions [58H, 77H], fibers [76H], wood [83H], shale [55H], and clay [56H]. The studies utilized models which predicted integral quantities such as drying time [86H], as well as finite-element methods which provided spatial temperature distributions [70H]. Researchers also consider the modeling of dryers [57H, 62H, 78H, 81H]. A control-volume method was used to reduce six partial differential equations in time and space to six ordinary differential equations in time. The approach was validated using a counter-current flow rotary dryer [57H]. Reynolds-averaged Navier–Stokes simulations were used to perform studies of turbulent flows in an impingement dryer [78H]. Researchers developed a time-dependent computational fluid dynamics model of the combustion processes in bagasse-fired furnaces [90H]. Finite-element methods were used to simulate the drying of ceramics which include volume change and hydrothermal stress [71H]. Neural network mapping was used to predict heat transfer coefficients in a fluidized bed [91H]. Finite-volume methods were utilized in performing simulations of grain drying in a cylindrical bed with evaporation boundary conditions [73H]. The effect of forced convective heat and mass transfer coefficients was investigated [59H]. A moving boundary model was developed to describe the frying of essentially 2-D objects [82H]. A mathematical model was developed for fluidized bed drying with microwave heating [88H]. The applicability of the infinite slab condition was assessed under a range of Biot and Fourier numbers [79H]. Stochastic modeling approaches were used in simulating heat and mass transfer in drying [61H]. Researchers also developed, and validated, a model of a single droplet in a two-phase flow inside a spray dryer [69H]. Additionally, a number of experimental investigations were also performed. In the drying of wood, temperature and weight measurements were used to calculate the position of the evaporation front beneath the surface [89H]. Several investigators considered the drying of foodstuff using different techniques [50H, 52H, 53H, 60H, 64H–66H]. These include fluidized beds [52H, 65H, 66H], and fryers [60H, 64H]. Researchers studied the design and performance of rotary dryers [67H, 87H], convective drying [63H, 84H], a combination of micro-wave and convective drying [74H], vacuum drying [80H], drying under turbulent flow conditions [54H], the performance of a mechanically spouted bed dryer [85H]. Researchers also measured gas velocities and moisture content in a con-

vective vacuum kiln in hopes of providing more uniform conditions [72H].

11.7. Miscellaneous

A variety of studies in which heat and mass transfer occurs in combination have been performed. These included the cooking of foods [112H, 113H, 132H, 136H, 138H], the modeling and analysis of wood pyrolysis [109H, 110H, 115H], combined heat and mass transfer and material surface characterization [97H, 98H], chemically reacting flows and combustion [99H, 100H, 103H, 111H], prediction of wood moisture content and subsequent combustion [117H, 119H, 140H, 141H], the removal of moisture from soils under various thermal conditions [102H, 104H, 108H], and multiphase transport [93H–96H]. Researchers also considered heat transfer mechanisms such as sublimation [116H], evaporation [130H], diffusion [139H] as well as both forced and natural convection [92H, 137H, 114H]. The coupling of the hydrodynamic and thermal fields was studied using both analytical and computational techniques [107H, 120H, 123H, 125H–128H]. Laser Doppler anemometry was used to measure temperature and velocity measurements in a heated jet interacting with a cold wire [124H]. Models were developed to predict erosion and moisture removal rates from soils [121H, 122H, 129H]. The transfer efficiency of oligomer ions in mono-component systems of polymer mixtures from solution phase to gas phase was examined [118H]. A non-equilibrium phenomenological theory of mass and heat transfer was developed and applied to ammonia synthesis [133H–135H]. Other studies include the development of a liquid crystal thermography for gas turbine heat transfer measurements [106H], estimation of the heat and mass transfer rates during the adsorption of volatile organic compounds [101H], modeling of water absorption in polyimide based composites [131H], and mass transport in a partially covered fluid-filled cavity [105H].

12. Bio-heat transfer

The bioheat transfer section of this review continues to evolve. The present review is still only a small portion of the overall literature in the area. This represents work presented in engineering journals with occasional basic science and biomedical journals such as *Cryobiology* and *Am. J. of Physiology*. This is a very dynamic and cross-disciplinary area of research, and thus, this review should be taken as more of an overview, particularly from an engineering point of view, rather than an exhaustive list of all work in this area for 2000. Subsections include work in *Cryobiology*, hyperthermia, thermoregulation and miscellaneous studies.

12.1. Cryobiology

Work in cryobiology can be broken in cryopreservation, crystallization/vitrification, and cryosurgery.

Cryopreservation work focused on CPA loading, freezing and thawing, and post freeze transplantation and use of biomaterials. In CPA loading, the precise quantification of CPA penetration in tissues as a function of time has been difficult, and a new MR approach to the characterization of cryopreservation permeation in an engineered dermal replacement was presented to address this need [3I]. Work in the area of freezing and thawing included characterization of a cryopreservation technique of precision-cut rat liver slices [10I] a cultured cartilage analog [12I]; assessment of ice morphology and recovery of chondrocytes in articular cartilage [11I] and the effect of temperature-dependent thermal conductivity in heat transfer simulations of frozen biomaterials [15I]. Rapid thawing of cryopreserved tissues by electromagnetic and conductive means was also studied [6I,9I]. Lastly, one study assessed vascular injury after transplantation of previously frozen mammalian livers [7I].

Work in the area of crystallization and vitrification (glass formation) included assessment of both intracellular and extracellular freezing events. One study assessed the effect of cell–cell contact on membrane integrity after intracellular freezing [11]. Other studies assessed the recrystallization inhibitor activity in plant and lichen species [5I] and the effects and mechanisms of antifreeze proteins during low-temperature preservation [Review] [16I]. Finally, vitrification studies showed enhancement by synthetic ice blocking agents [17I] and the tendency of a glass to form in the system water–dimethyl sulfoxide was also assessed [2I]. The phase diagram, including glass forming information for trehalose–water binary mixture was also presented [4I].

In cryosurgery, the use of freezing *in situ* was used to control hemorrhage from liver injury [8I] and as an experimental treatment for thyroid [13I]. Cryosurgical probe characterization studies were also performed for general freeze/thaw processes around a probe [19I] and in porcine and human liver tissue and human colorectal liver metastases *in vitro* [14I]. Finally, an *in vitro* monitoring system for simulated thermal processes in cryosurgery and ensuing damage was also presented [18I].

12.2. Hyperthermia

Work in this area can be broken into thermal therapies, adjuvants, heat death mechanisms and kinetics, and bioheat transfer modeling.

Thermal therapy continues to be an area of active work due to the minimally and at times non-invasive nature of high-temperature tissue destruction afforded by new equipment. Several studies using micro-wave,

Radio-Frequency RF, High Intensity Ultrasound (HFU) and Laser have been reported. Micro-wave and radiofrequency studies report a new 434 MHz interstitial hyperthermia system monitored by micro-wave radiometry [22I] and a dielectric-loaded coaxial-slot antenna for interstitial micro-wave hyperthermia [30I]. Further characterization studies show that the position, size and distance of the opposite applicator changes the SAR and thermal distributions in some RF applications [31I,32I]; and resonance effects in applicator water boluses can also affect the SAR [28I]. Characterization work in HIFU assessed cylindrical ultrasound transducers for intracavitary hyperthermia [35I] and temperature elevation at the muscle/bone interface [36I]. Further ultrasound work investigated the treatable domain and optimal frequency for brain tumors [37I]. Several characterization studies looked at the effects of cavitation bubbles on US lesions [23I] and the directional power deposition from direct-coupled versus catheter-cooled interstitial US applicators [40I]. In the laser area, an analysis of cryogen spray cooling during laser treatment of port wine stains was presented by [43I] and [52I] and the temperature change in teeth at the dentin/pulpal interface was assessed [25I]. Lastly, one study reports the use of hyperthermia and radiotherapy for inoperable squamous cell carcinoma [20I].

Adjuvants to heat destruction were also studied. Potential adjuvants included local anaesthetics [49I]; granulocyte-colony stimulating factor [50I]; paclitaxel–epirubicin chemotherapy [24I]; and heat with cancer cell cytosol immunization [41I]. Heat-inducible vectors for use in gene therapy were also investigated by Gerner et al. [29I].

The mechanism of heat death and/or kinetics were studied by several groups in various systems. Studies included: supraphysiological thermal injury in Dunning AT-1 prostate tumor cells [21I]; thermal death kinetics of insect pests [33I] and apoptosis induced by hyperthermia in Dunn osteosarcoma cell line [48I]. It was also found that fever-range hyperthermia stimulates alpha4beta7 integrin-dependent lymphocyte-endothelial adhesion [27I]. The injury outcome of hyperthermia on tissue was assessed after interstitial therapy on normal rat brain by histology [34I] and after whole body by assessment of murine leukocyte populations [42I]. Lastly, one study showed that thermotolerance (and rapid cold hardening) ameliorate the negative effects of brief exposures to high (or low) temperatures on fecundity in the flesh fly, *Sarcophaga crassipalpis* [46I].

Modelling of temperature excursion in the body, particularly during hyperthermia with blood flow, continues to be an area of intense activity using the bioheat equation. Modelling included assessment of perturbations in hyperthermia temperature distributions associated with counter-current flow [26I]; temperature profiles in an isolated perfused bovine tongue [44I]; use

of a discrete vessel model in thermal simulations [45I]; temperature simulations in tissue with a computer generated vessel network [51I]; an energy equation based automated meshing technique for analysis of blood vessels and tissues [53I] and heat transfer to the periodontal ligament during root obturation [47I]. Other work investigated the morphometry of the canine prostate vasculature to assist in the blood flow term of the bioheat equation [54I] and boundary information based diagnostics on the thermal states of biological bodies [39I]. Additionally, the controversial subject of whether heat transfer in living tissues exhibits wave-like behavior was reviewed by Liu [38I].

12.3. Thermoregulation

Work in this subarea included heating, cooling and general studies as well as studies related to clinical operations. Heating work included discussion of effects of whole body heating on dynamic baroreflex regulation of heart rate in humans [58I] and heat production in human skeletal muscle at the onset of intense dynamic exercise [59I]. It was also shown that pre-treatment with mild whole body heating prevents gastric ulcer induced by restraint and water-immersion by stress [61I]. Other work modeled heat mat operation for piglet creep heating [74I] and the effect of acute heat exposure on skin blood flow in persons with paralysis [72I].

Cooling work included the integrated response of the upper and lower respiratory tract of asthmatic subjects to frigid air [62I]; a new approach to calculation of wind chill [63I] and the effects of phase control materials on hand skin temperature within gloves of soccer goalkeepers [64I]. Additional studies investigated hemorrhage-induced hypothermia and the accompanying reduced metabolic rate in rats [60I] and skeletal muscle properties in cadaveric test specimens after freezing [71I].

General work included the evaluation of cutaneous heat flux model limitations for metabolic rate studies of marine mammals [56I]; thermal analysis and design of an advanced space suit [57I]; generation of an anatomically based 3-D model of the conducting airways [66I]; parametric studies of human thermal mechanisms and measurements [67I]; thermal balance of livestock [70I]; heat transfer in the micro-vascular network in reptiles [65I] and steady and pulsatile flow studies in Abdominal Aortic Aneurysm models [73I].

Studies relevant to clinical thermoregulation included the implications of packed cell volume on specific heat measurements for heat exchange in extracorporeal circuits during anesthesia [55I]. Additional work assessed thermal and hemodynamic responses to postoperative rewarming with a sub-atmospheric pressure device [68I]; measurement of porcine heart temperatures [69I]; conceptual design of a combined device for normothermia

and venous compression [75I]; and a theoretical evaluation of contributions of heat conduction and counter-current heat exchange in selective brain cooling in humans [76I].

13. Change of phase – boiling

Thermal transport phenomena associated with liquid-to-vapor phase change are addressed in the publications reviewed in this section and classified into five major categories: droplet, film, and explosive evaporation (23 papers), bubble characteristics (15 papers), pool boiling (44 papers), flow boiling (32 papers), and two-phase thermohydraulics (12 papers). In addition to these 126 papers, the interested reader will find reference to studies of evaporative and ebullient heat transfer among the papers included in: change of phase – condensation (JJ), heat transfer applications – heat pipes and heat exchangers (Q), and heat transfer applications – general (S).

13.1. Droplet and film evaporation

The 2000 archival literature provides several fundamental studies of droplet evaporation, including the effects of a vortex and acoustic fields, respectively, [12J,19J], evaporation of binary liquid droplets [8J,14J], droplet evaporation in a supercritical environment [3J,23J], and the impact dynamics and heat transfer for a saturated drop impinging on a heated surface in the non-wetting regime [9J].

Evaporation of liquid films is described in [16J] – dealing with a liquid fuel evaporating from a metal substrate, in [15J] – presenting the development of a phenomenological model for an evaporating meniscus, in [1J] – emphasizing the development of expressions for eddy diffusivity in turbulent falling films, in [21J] – offering a new, computationally efficient model for multi-component evaporation, and in [17J] – providing accurate approximations for intensive evaporation. The effects of surfactants on evaporation from an open water surface are described in [18J], evaporation from the wetted floor of an open cylinder in [13J], the evaporation of refrigerant films in a vapor compression cycle in [2J], and the experimental heat transfer characteristics of refrigerant–oil mixtures in evaporator tubes in [6J].

Evaporation during vapor explosions is described in [4J] – providing two distinct models for this phenomenon, in [5J,7J] – dealing with flashing in tubes, and in [22J] – with explosive vaporization on a micro-heater. The development of a new spray/wall interaction model [10J], along with the use of water sprays to cool glass fibers [20J] and die-cast steel rods [11J], is also described in the 2000 literature.

13.2. Bubble characteristics

Single bubble characteristics underpin much of the modeling and understanding of ebullient heat transfer. Heat transfer and fluid flow in a non-isothermal constrained vapor bubble is studied in [29J], parametric effects on bubble coverage on electrodes in [26J], characteristics of bubbles generated on micro-heaters in [37J], bubble dynamics during pool boiling in [35J,36J], bubble dynamics in high-frequency acoustic fields in [27J], bubble behavior in a uniform electric field in [38J] and heat and mass transfer during the rise of superheated bubbles in [24J,25J], velocity of long bubbles in oscillating pipes [30J], and numerical simulation of bubble rise at elevated pressures in [32J]. The characteristics of collapsing bubbles attracted the attention of [28J] – exploring the effects of non-uniform flow, of [34J] – dealing with binary mixtures, of [33J] – describing molecular dynamics computer simulations, and of [31J] – studying collapse driven micro-bubble emission boiling.

13.3. Pool boiling

Fundamental studies of pool boiling behavior continued to attract the attention of the heat transfer community, with a notable focus on the characterization of the active nucleation sites [62J] and the interaction among neighboring nucleation sites [41J–43J,65J], as well as the effect of surface roughness [52J]. The results of an exploration of multiple solutions for boiling on a wire are reported in [80J] and the influence of heat conduction in the wall in [66J].

Several of the pool boiling heat transfer studies in the 2000 literature deal with important extensions of the ebullient transport knowledgebase to include the correlation of pool boiling of halocarbon refrigerants [73J], effects of heater orientation and confinement [68J], boiling from a downward facing surface [51J], transient heat transfer [64J], cyclic heating [47J], effects of microgravity on micro-scale boiling [76J], and the influence of mass transport during the boiling of multi-component mixtures [55J].

The thermal design and optimization of pool boiling fins was explored in several studies, notably in [60J] – addressing both the stable and metastable regimes, in [46J,61J] – examining boiling of dielectric liquids from single fins, and in [39J] – exploring issues in the design of boiling heat sinks for immersion cooling of electronics. The literature also provides results for the augmented boiling of refrigerants on the Turbo-BII-HP tube [77J] and grooved tubes [71J], as well as for the addition of hydrocarbons [53J].

Fundamental aspects of pool boiling on porous surfaces are described in [59J] and [82J], while the effects of oil on the boiling of refrigerants and the boiling

of mixtures in [81J] and [72J], respectively. Pool boiling of distilled water on a PTFE-coated tube is described in [78J]. Enhancement of pool boiling with electric fields is addressed in [44J] – exploring EHD effects on finned tubes, in [57J] – visualizing the benefits of non-uniform dc electric fields, in [69J] – comparing the behavior of several fluids, and in [75J] – investigating the effectiveness of an electric field in microgravity.

In boiling heat transfer, the Critical Heat Flux (CHF), or “boiling crisis”, represents the heat flux value at which vapor blankets the heater surface and the heat transfer coefficient deteriorates. The 2000 literature includes an experimental study of dryout in a falling film [79J], CHF in an open thermosyphon [67J], and CHF on a laser heated thin plate [48J], as well as a theoretical derivation of the critical heat load [56J] and of a dry-spot based model of CHF [49J].

A broad review of theoretical models and the experimental literature on the transition from CHF to film boiling, along with recent experimental results on the temperature distribution adjacent to the film boiling boundary is provided in [63J,74J], respectively. Trans-CHF behavior, as encountered in quenching of samples in water [58J], freezing of biological samples and food [50J], and under severe reactor accident conditions [40J] is also described. Models of film boiling in superfluid helium under microgravity conditions are examined in [45J,54J]. An extensive development of thin-film asymptotics is used to provide the theoretical foundation for horizontal film boiling in [70J].

13.4. Flow boiling

The broad range of interactions between a pumped flow of liquid and vapor bubbles generated and released on a heated surface provides a large number of flow boiling heat transfer mechanisms and a diverse flow boiling literature. Several of the studies contained in the 2000 archival literature deal with the onset of nucleate flow boiling in horizontal tubes [114J], minichannels [92J], microchannels [102J], and in finned, annular channels [108J]. Others, expand the use of the available correlations to unconventional fluids, such as kerosene [87J], HFC refrigerants [86J], and wide-boiling binary and ternary mixtures [112J]. The influence of the flow boiling flow regime on the temperature distribution of a heated wall is investigated in [93J].

During 2000, the literature has been enriched by studies of the thermohydrodynamic characteristics of flow boiling in various channel geometries, including microchannels [85J,100J,101J], narrow refrigerant passages [84J], annular ducts [113J], hot-rolled wires [99J], channels in a die for pressure die-casting [88J], and a horizontal geologic fracture [111J]. Flow boiling in en-

hanced surface tubing was examined in [103J–106J], while enhancement due to a screen sheet suspended in the flow was the subject of [94J].

The archival literature of 2000 provides evidence of further progress in the understanding and enhancement of the flow boiling “crisis”, including both critical heat flux and dryout. Hall and Mudawar [90J,91J] provide a comprehensive review of CHF for water flowing in tubes. A CHF model for subcooled flow boiling, which is extendable to non-uniform heating, twisted tape inserts and other fluids, is presented in [97J], while a modeling approach for square rod bundles is articulated in [95J] and experimental data for CHF on protruding and flush-mounted simulated chips is presented in [110J]. The influence of subcooling on the relative stability of nucleate boiling and film boiling on an inclined surface is explored in [96J].

The correlation and modeling of post-CHF, dispersed-flow film boiling in tubes [107J] and in the core of a nuclear reactor [83J], convection-controlled film boiling along fast moving wires [98J] and along a vertical cylinder [109J], as well as a detailed examination of the liquid–wall contact characteristics adjacent to a quench front [89J] are also reported.

13.5. Two-phase thermohydraulics

The design of flow boiling systems must include attention to the thermohydraulic aspects of two phase flow. The accurate prediction of pressure drop in two-phase flow continues to occupy many researchers and led to the publication of a review of phenomenological models for the pressure gradient in horizontal gas–liquid flows [124J], horizontal pipe pressure gradient and hold-up data for low liquid loadings [116J], experimentally determined two-phase flow patterns and pressure drop in micro-rod bundles [121J], and pressure drop measurements for refrigerants in small channels [123J].

The transition from slug to annular flow in micro-gravity was the subject of [126J], while [120J] described the measurement of void fraction in magnetic two-phase fluids, and [117J] presented a methodology for the prediction of slug liquid hold up in vertical flows. The prediction of acoustic wave velocities in two-phase flows was described in [125J].

Droplet characteristics are central to the understanding of thermal transport in annular and wispy annular flow. Several distinct droplet models are used in [115J] to underpin the numerical prediction of depressurization of highly pressurized propane, while [118J] provide evidence for the existence of core structures in high-mass flux annular flows, [119J] provide a correlation for the droplet entrainment rate, and [122J] discuss the use of an isokinetic probe for establishing droplet flow parameters.

14. Change of phase – condensation

Papers on condensation published during 2000 are separated into those which deal with surface geometry effects; those on the effects of global geometry, thermal boundary conditions and external influences; papers presenting techniques for modeling and analysis; papers predominately on free-surface condensation; papers on unsteady effects and papers dealing with mixtures.

14.1. Surface geometry and material effects

Papers on the importance of surface geometry to condensation include one on the effects of coiled wires inserted into horizontal tubes [1JJ]. It shows a 100% improvement in heat transfer coefficient over smooth tube performance. Five papers discuss micro-finned tube performance [2JJ,3JJ,5JJ,7JJ,8JJ]. Micro-fins of axial, helical and cross-hatch geometries are evaluated [7JJ, 8JJ] to learn that the cross-hatched geometry performs best with several refrigerants. Another study, presented in two similar papers, compares condensation with smooth and micro-finned tubes using R22 [2JJ,3JJ]. The importance of surface tension forces when the vapor quality is high is discussed. A study of condensation with two refrigerant types in smooth and herringbone-type, micro-finned tubes is presented [5JJ] in which it is noted that the herringbone-type geometry provides higher heat transfer coefficients, and pressure drops. The effects of surface waviness on a disk facing upward is discussed with respect to laminar film condensation [4JJ]. The wavelength and amplitude of the surface waviness, and suction through the surface, play important roles in determining film thickness. Finally, mass transfer from the surface of the sea is measured [6JJ] and analyzed. The assumption that the roughness length is the same for modeling both heat and moisture transport is assessed.

14.2. Global geometry, thermal boundary condition and external influence effects

Papers which describe the effects of global geometry include three with vertical tubes and surfaces [16JJ,18JJ,25JJ], eight with horizontal and inclined tubes and surfaces [9JJ], and [11JJ,17JJ,20JJ–24JJ], a helical tube, [15JJ] and several system or device-oriented papers [10JJ,12JJ–14JJ,19JJ]. Experiments are conducted to assess the effects of non-condensables in passive cooling systems of nuclear reactor containments using a vertically mounted, smooth tube [18JJ]. The gas stratification phenomenon is clearly observed when the gas mole fraction exceeds 60%. For the same application, a study develops a new turbulent annular film condensation model for steam in a vertical tube [16JJ]. Pure saturated vapor condensation with downward flow over a

horizontal cylinder or cylinder bank is numerically studied where particular attention is given to the effects of surface tension [9JJ]. A model is developed for forced convection condensation in the annular flow region between horizontal tubes [17JJ]. Comparisons within 30% on mass flux with the data are achieved. A similar study is with an adiabatic inner tube [23JJ]. The analysis shows that the effects of surface tension cannot be neglected when the tube is small. A similar study, but with inclined tubes, is presented [24JJ]. Condensation in horizontal tubes with several HFC refrigerants is experimentally assessed and the results are compared with correlations [11JJ]. One correlation is noted to give the best comparison. Condensation of pure and azeotropic fluids in smooth horizontal tubes is documented, including the flow pattern changes with flow conditions and fluid type [21JJ]. Zeotropic (or non-azeotropic) refrigerant mixtures are investigated in a similar geometry [22JJ]. A prediction method for pressure drop and heat transfer rates in the same geometry is presented [20JJ]. Standard design models are tested. Helicoidal tubes are tested with R134a inside [15JJ]. The data are compared to those with a horizontal straight pipe. Condensation in gas-fired boilers of water from the products of combustion is documented [14JJ]. The models predict fin efficiencies below those obtained using an assumption of constant heat transfer coefficient and temperature. Droplet condensation of metal vapor on the under side of a stainless steel plate is studied [19JJ]. Scanning electron microscopy of the droplets formed is the recommended visualization method. Two papers are on steam-driven jet pumps. In one, a mathematical model is presented [10JJ]. Key to the analysis is the modeling of the nozzle. Visualization in jet pumps is carried out [13JJ]. The intent is to better understand the physical laws driving the flow. A prototype of an adsorption refrigerator which uses a carbon–aluminum laminate absorber surface is tested with emphasis on assessing the intensification of heat transfer within the bed [12JJ].

14.3. Modeling and analysis techniques

Conjugate condensation-heat conduction analysis is applied to a vertical fin geometry and the equations are written in terms of Prandtl and Jakob numbers, a non-dimensional fin thermal conductivity ratio and the aspect ratio [29JJ]. The Graetz problem, but applied to condensation, and with wall conduction, is applied to analyze condensation on the external surfaces of two vertical thin plates [26JJ]. In addition to the parameters of the previous paper, the ratio of thermal conductance of the condensed layer to the thermal conductance of the forced cooling flow is added. A numerical method is applied to condensing steam flow within a compressible boundary layer [32JJ]. Viscous dissipation and reduced

expansion rates within the boundary layer are shown to influence nucleation and growth of the droplets relative to those predicted with inviscid flow. Droplet size distributions are modeled for condensing steam using the moments of the size distribution [33JJ]. Two papers deal with nuclear reactor modeling using RELAP5. In one, the code is interrogated regarding the models for thermal stratification, condensation and natural circulation flow with the small driving forces present in the small break accident [31JJ]. Another paper investigates numerical diffusion [30JJ] in the code. The authors note that automatic halving of the time-step can lead to failure of the accuracy of simulation. An automobile air conditioner is simulated as a system and the effects of condenser size and refrigerant charge on the performance are discussed [28JJ]. A new theory is developed for adsorption chiller units to describe why surfactants in the fluid, added for boiling improvement, also improve condensation [27JJ]. The conclusion is that the surfactants generate intense Marangoni secondary flow circulation due to surface tension gradients.

14.4. Free-surface condensation

Two papers specifically focus on free-surface condensation. In one, condensing bubbles make uniformly sized liquid droplets. The bubbles form by injecting vapor in an immiscible liquid [35JJ]. A model is developed to estimate direct contact condensation of steam bubbles [34JJ]. Measurements are made by using holographic interferometry. Maps of the results show that the boundary between chugging flow and subsonic jetting is shifted to larger steam mass flux values when the pipe size is increased.

14.5. Unsteady effects in condensation

One paper on unsteady effects analyzes experimental data on the formation of aromatic species from sooting flames [39JJ]. Measurements of pyrolysis, partial oxidation and combustion of acetylenes as well as allene and ketene in turbulent flow reactors, jet-stirred reactors and shock tube experiments are used in the analysis. Nucleation of aerosols in laminar tube flow is analyzed with approximate methods in terms of the Lewis number and a parameter which describes the temperature variation of the equilibrium vapor concentration [37JJ]. The predictions are shown to agree with numerical results. Condensation-induced water hammer is addressed experimentally and analytically [38JJ]. The analysis uses an improved criterion for transition from stratified flow to slug flow. The effects of non-condensables on the unsteady flow by natural circulation inside horizontal tubes are assessed experimentally [36JJ]. The results show a blockage of heat transfer area by the gas which leads to increased primary pressure, followed by com-

pression of the gas and re-entry of the steam, hence the dynamics.

14.6. Binary mixtures

Papers which deal with mixtures include one which shows the effects of additives to R123 on condensation [41JJ]. A 0.5% by mass isopentane addition improves pool boiling. Previously the effect on condensation had not been assessed. On average, a 4% reduction in performance was experimentally found. The degradation was presumed to be by the zeotropic behavior of the mixture, which leads to a loss of available driving temperature difference for heat transfer across the film. In three similar papers, a method for prediction of condensation of azeotropic mixtures in horizontal, enhanced-surface tubes is employed [44JJ–46JJ]. Both pressure drop and heat transfer are included. The papers differ in the fluid used for testing. Analysis of the trapping of impurity molecules in material deposition from mixtures of gases is investigated [42JJ]. Trapping is correlated with the condensation. Condensation in boundary layers, as affected by non-condensable gases, is discussed [40JJ]. Fog forms within the steam-nitrogen boundary layer and steam condenses at the water droplets' surfaces; then the fog layer no longer reaches the cooling water interface and condensation is reduced. Condensation of potassium salts in straw-fired boilers is experimentally investigated [43JJ]. A novel probe is designed for this investigation.

15. Change of phase – freezing and melting

This is the change of phase (freezing and melting) section of the review. It is broken into several subsections including: melting and freezing of sphere, cylinders and slabs; Stefan problems; ice formation/melting; contact melting; melting and melt flows; powders, films, emulsions and particles in a melt; crucible melts; glass technology; welding; enclosures; nuclear technology; energy storage – PCMs; casting, moulding, and extrusion; mushy zone – dendritic growth; solidification; crystal growth; droplets, spray and splat cooling; oceanic and geological phase change and miscellaneous.

15.1. Melting and freezing of sphere, cylinders and slabs

In this section, work on freezing in several geometries was pursued. In slab geometry, freezing during quenching was investigated [4JM]. In cylindrical geometry water freezing in a horizontal circular cylinder [5JM], and high-pressure freezing in a cylinder [3JM] were investigated. In addition, freezing with flow in both parallel-plate laminar conditions [2JM] and Couette cylinder flow in an annulus were reported [1JM].

15.2. Stefan problems

Stefan problem work was reported by several groups. Numerical solution of one-phase Stefan problems by the heat balance integral method in cylindrical and spherical geometries was reported [6JM]. In addition, electron-beam autocrucible melting was studied by means of the steady-state Stefan problem [7JM]. Analytical modeling of transient phase-change problems was reported [8JM], and with a generalized Stefan problem approach to fluvio-deltaic sedimentation was reported by [9JM].

15.3. Ice formation/melting

Ice formation and melting was studied in or on food, soil, wastewater, aircraft applications and general solid surfaces as well as in several miscellaneous systems. In foods, freezing and thawing was studied by a modified fictitious heat flow method [12JM], and a neural network technique [18JM]. Convection and solidification in food freezing was also studied in a plate shaped food [19JM] and in food within a freezing chamber [20JM]. In soil, heat and mass transfer in columns during freezing/thawing was studied [22JM]. In wastewater, treatment using an in situ freezing–melting process was studied by Hirata et al. [11JM], and the freezing temperatures of freely falling industrial wastewater droplets was studied by Gao et al. [13JM]. In aircraft applications, glaze or ice growth on airfoils was studied by Politovich [23JM] and anti-icing was studied by Morency et al. [21JM]. Other studies of ice formation on solid surfaces included: time to the onset of ice formation at metal surface [10JM] and the effect of concentration gradient on the melting of a horizontal ice plate from above [24JM]. Further studies report on ice formation and removal on cooled horizontal solid surfaces [14JM,15JM]. Miscellaneous studies report on the sublimation and vaporization of an ice aerosol by laser radiation [17JM] and solid–liquid equilibria of organic binary mixtures [16JM].

15.4. Contact melting

Contact melting of a pure metal on a vertical wall was numerically simulated by Stella and Giorgi [26JM]. Analytical solutions to unsteady close-contact melting on a flat plate were also presented [27JM]. In addition, melting from heat sources flush mounted on a conducting vertical wall was analyzed [25JM].

15.5. Melting and melt flows

The work in this category can be subdivided into steel and metal melt, laser processing, magnetic field effects, and general melt flow modeling. Steel and metal melt work included modeling of steel flow in a Tundish

heated by plasma [28JM]; effects of buoyancy and flow control of liquid steel in a Tundish [38JM]; kinetics of steel scrap melting in molten Fe–C bath [31JM]; effect of molten steel flow on the solidification shell [44JM]; melting and dissolution of low-density ferro-molybdenum in steel melts [41JM]; inclusion removal and microstructure in electron beam button melting [32JM] and modeling of a molten zinc pot of a continuous hot-dip galvanizing line [36JM]. Melt studies in laser processing included shape changes of colloidal gold nano-rods using femtosecond and nanosecond laser pulses [37JM] and delayed melting at the substrate interface of amorphous Ge films [43JM]. Magnetic field effects were studied in the dynamics of semi-levitation melting [30JM] and in an oxide melt [34JM]. General melt flow work included: thermocapillary flow in a jet of liquid (melt) film painted on a moving boundary [33JM]; study of slipping fluids by a unified transient network model [35JM]; modeling of molten material–vapor–liquid mixtures in thermal non-equilibrium [42JM]; and thermofluid analysis of the entrance section of a continuous pressure infiltration process for fiber–metal matrix composites [40JM]. Additional studies on the melt behavior of float zones in micro- and low-gravity environments [29JM] and for thermal management of high-power electronics with phase-change cooling [39JM] were presented.

15.6. Powders, films, emulsions and particles in a melt

Studies in this section were dominated by particle-laden melt work. These included convective stability of a particle-laden fluid system in the presence of solidification [45JM]; lattice–Boltzmann simulations of fluidization of rectangular particles [46JM]; and modeling of the iron ore sintering process including the agglomeration phenomenon of granules in the packed bed [47JM]. In addition, investigation of coatings and SiCf/SiC composites under thermal shock were reported [48JM].

15.7. Crucible melts

See work described in Section 2 by [7JM].

15.8. Glass technology

Glass melting work included modeling of an industrial glass-melting furnace [49JM]; melting using an IGBT full bridge resonant converter [50JM] and investigation of means of increasing the energy efficiency and intensity of glass melting [51JM,52JM].

15.9. Welding

Welding work included analysis of single-pass arc welds [53JM]; fusion welding [54JM]; resistance spot

welding in aluminum [55JM]; and micro- and macro-modeling of titanium arc welding [56JM].

15.10. Enclosures

See studies in Section 12.

15.11. Nuclear technology

Phase-change work in nuclear technology included an implicit enthalpy formulation for oxidation of nuclear reactor fuel cladding by steam [57JM], and investigation of heat removal from a liquid–salt target irradiated with high-energy protons [58JM].

15.12. Energy storage – PCM

Studies in this section investigated the storage and release of energy during a phase-change process. This included the investigations included the investigation of thermal characteristics of paraffin in a spherical capsule during freezing and melting processes [59JM]; solidification of phase-change material (PCM) inside a spherical capsule [60JM]; and melting of a phase-change material in a concentric horizontal annuli [61JM].

15.13. Casting, moulding, and extrusion

Work in this section was dominated by casting with some moulding and extrusion reports. The casting work included thermal analysis during continuous casting using an effective heat capacity method [62JM]; modeling of defects in shape castings based on various effects [63JM]; modeling microporosity formation in aluminum alloys due to various effects [66JM]; speed disturbance compensation in continuous casting [64JM]; and analysis of microstructural characteristics in sand cast Al–Si alloys [69JM]. Modeling work in steel and alloy casting analyzed grain selection during the solidification of single crystal superalloy castings [65JM]; fluid flow phenomena during Tundish filling and casting [68JM]; fluid flow, heat transfer, and solidification in two-roll melt drag thin strip casting of steel [70JM]; thermally induced stresses in two-roll melt drag thin strip casting of steel [71JM]; and instantaneous heat fluxes from solidifying steels to the surfaces of twin-roll casters [72JM]. Further modeling work in casting included simulation of coupled turbulent flow and heat transfer in the wedge-shaped pool of a twin-roll strip casting process [74JM]; application of the boundary element method for the modeling of cylindrical and spherical castings [77JM]; an asymptotic approach to the mathematical modeling of Ohno continuous casting of cored rods [78JM]; and numerical analysis of fluid flow and heat transfer in the funnel type mold of a thin slab caster [79JM]. Other work in the area included investigations into the effects

of processing parameters on the microstructure and mechanical properties of alloy in direct squeeze casting [76JM] and the mechanisms of initial melt/substrate heat transfer pertinent to strip casting [80JM]. Finally, one study focused on finding appropriate boundary conditions for the modeling of metal casting [83JM].

Work in the moulding area included modeling of phase change and material performance in blow moulding and thermoforming [67JM]; predicting stereolithography injection mould tool behavior [73JM] and modeling temperature distributions in cooling chocolate moulds [82JM].

Modeling to predict the plasticating [75JM] and non-isothermal flow of polymer melts [81JM] in single screw extruders were also presented.

15.14. Mushy zone – dendritic growth

Investigations into the behavior of the mushy zone or dendritic growth processes in impure material phase-change processes included modeling of interdendritic strain and macrosegregation [84JM]; a model of microsegregation during binary alloy solidification [85JM]; and the effect of free-floating dendrites and convection on macrosegregation in cast aluminum [86JM,87JM].

15.15. Solidification

Solidification work, predominantly in metals, involved a considerable number of studies on interfacial heat transfer, rapid solidification as well as general phenomena surrounding phase change in metals.

Interfacial work included studies on heat transfer and heat transfer coefficients. Interfacial heat transfer was studied during nucleation of steel-on metallic substrate [89JM] and for design and control of interfacial temperature gradients in solidification [92JM]. Interfacial heat transfer coefficient determination was carried out during unidirectional solidification of an aluminum alloy [90JM]; unidirectional Al–7 wt%Si alloy solidification with special geometry [91JM]; on the solid–fluid boundary with the phase change in a fluid [93JM]; at the metal–mould interface in the unidirectional solidification of Cu–8%Sn alloys [96JM] and also with a thermal stress model [94JM].

Work primarily concerned with the effects of rapid solidification included studies on multi-stage rapid solidification [95JM]; micro-scale heat and mass transfer during non-equilibrium phase change [97JM]; a model of dendritic and planar interface growth and morphology [98JM]; shape of a pore trapped in solid [99JM] and non-equilibrium planar interfaces during solidification of radiating materials [100JM].

Studies of generalized phenomena during solidification reported an algorithm for modeling phase change problems in materials processing [88JM]; multi-

dimensional solidification with internal radiation and temperature-dependent properties [101JM]; the effect of viscous plane stagnation flow on the freezing of fluid [102JM]; and a model of solidification in inviscid stagnation flow [103JM].

15.16. Crystal growth

Investigations in this area can be divided into vertical zone, polymer and melt spinning, Czochralski, Bridgman and general crystal growth studies.

Work on vertical zone crystal growth reported on the effects of axial vibration on melt processing [115JM]; 3-D simulation of crystal growth with symmetry [116JM]; weak transverse magnetic field and crystal rotation [120JM] and dopant distribution in Ge single crystals grown aboard spacecrafts [113JM].

Polymer solidification and crystal growth work included directional solidification of isotactic and atactic polypropylene blends [112JM]; simulation of crystallization in high-density polyethylene [124JM]; modeling of the melt spinning of polyethylene terephthalate [123JM] and simulation of melt spinning including flow-induced crystallization [106JM].

Czochralski crystal growth work included modeling of a CZ melt using a block-structured finite-volume method [104JM]; influence of Marangoni convection on the flow pattern in the melt during growth of $Y_3Al_5O_{12}$ single crystals [109JM]; crystal–melt interface shape in the growth of oxide single crystals [111JM]; effect of internal radiative heat transfer on CZ oxide melt [114JM]; a hybrid finite-volume/finite-element simulation of heat transfer and melt turbulence in growth of silicon [118JM] and numerical simulation for silicon crystal growth of up to 400 mm [127JM].

Bridgman crystal growth work included investigation of vibrational control of convective flows in melt growth configurations [107JM]; simulation of growth in a material with anisotropic solid-phase thermal conductivity (i.e. benzene) [117JM]; boundary element modeling of the growth process of semi-transparent crystals [119JM]; the influence of gravity levels on the horizontal Bridgman crystal growth of an alloy [126JM] and a computational study of transient plane front solidification of alloys under micro-gravity conditions [128JM].

General crystal growth work included in situ visualization of $Cd_{1-x}Zn_xTe$ nucleation and crystal growth [105JM] and X-ray visualization of silicon carbide vapor transport [130JM]. Additional work on the solidification of Ga–Mg–Zn in a gas-filled drop [108JM]; mold surface wavelength effect on gap nucleation [110JM]; silicon carbide crystal growth by physical vapor transport method [121JM]; void engulfment in shaped sapphire crystals [122JM]; impurity distribution in semiconductor crystals [129JM]; edge-defined film-fed growth process [131JM] and the influence of

electromagnetic field on resistivity variations in Si single crystals [125JM] were presented.

15.17. Droplets, spray and splat cooling

Work on molten droplet and sprays included a number of studies on solidification of droplets along with other liquid-phase analysis. These included simulation of metal droplet deposition with solidification [133JM]; liquid droplet solidification on substrates [136JM]; spreading and solidification of a molten metal droplet on a cooled substrate [138JM]; liquid metal particles impacting onto solid [140JM]; and droplet-based deposition [141JM]. Additional work included the analysis of impact, recoil and splashing of molten metal droplets [132JM]; interaction of a molten droplet with a liquid weld pool surface [134JM]; iron drop ejection into slags by bursting gas bubbles [135JM]; effects of thermocapillary convection on melting within droplets [137JM]. In addition, in situ temperature measurement during spray forming of A2-tool steel and axisymmetric 2-D analysis was presented [139JM].

15.18. Oceanic and geological phase change

Predominantly magma studies were presented in this section including deformation and freezing of enclaves during magma mixing [142JM]; extended-Boussinesq thermal-chemical convection with moving heat sources and variable viscosity [143JM]; simultaneous crystallization and melting at both the roof and floor of crustal magma chambers using $\text{NH}_4\text{Cl-H}_2\text{O}$ binary eutectic system as a model [144JM].

15.19. Miscellaneous

Variational methodology using the enthalpy of the system to model heat flow and phase change within a structure of random material properties was also presented [145JM].

16. Radiative heat transfer

The papers below are divided into subcategories, which focus on the different impacts of radiation. Most of the papers report the results of modeling studies. Papers describing the development of new numerical methods themselves are reviewed in the numerical methods section under the subcategory radiation.

16.1. Influence of the geometry

The most striking observation in this section is the decrease of papers dealing with the determination of view factors. Katte and Venkateshan [3K] derive view

factors in axisymmetric enclosures containing shadowing bodies.

One-dimensional sphere packings for sintering are considered in [12K]. Two-dimensional irregular enclosures are considered in [1K,9K]. Three-dimensional radiation problems are studied in [4K,7K,10K]. An unstructured radiation model for 2- and 3-D problems is proposed by Liu et al. [5K].

Monte Carlo radiation models are used to model thermal radiation in semiconductor processing [6K]. Circular infrared lamps used in rapid thermal processing are studied in [2K]. The influence of radiation on the meteorological conditions in urban canyons is studied in [8K,11K].

16.2. Radiation and combustion

Combustion problems involve radiative heat transfer as well as participating media, and other heat transfer modes. The increase in the number of publications over the last years justifies grouping these papers in a separate section.

A number of papers consider radiation in flames. Diffusion flames are studied by Liakos et al. [24K], Morvan et al. [28K], and Olson and Tien [29K]. The inverse radiation problem of axisymmetric free flames is studied by Liu et al. [26K]. Radiation extinction of stretched premixed flames is studied by Ju et al. [18K].

Radiation in fires is studied by several authors. Turbulent burning between vertical walls with fire-induced flow is considered in [33K]. The spectral formulation for radiative transfer in 1-D fires is studied by Demebele and Wen [16K]. Soares and Teixeira [31K] report probabilistic modeling of offshore fires. Lilley [25K] investigates the minimum safe distance from pool fires. Ray effect mitigation in jet fire modeling is studied in [15K].

Radiation is also important in the study of furnaces. Fluidized bed-like furnaces are considered in [13K], coal-fired furnaces are investigated in [27K,32K], and natural gas fired furnaces are the subject of [20K,21K]. Radiative transfer in controlled-atmosphere furnaces is studied by Ratts [30K]. Radiation in a 0.3 Mwt Atmospheric Fluidized Bed Combustor test rig is studied by Kozan and Selcuk [23K].

Kayakol et al. [19K] simulate gas turbine combustors. Chen et al. [14K] perform multi-dimensional simulations of direct injection Diesel engines. Radiation properties of combustion products are reported in [22K]. Ewald et al. [17K] investigate the combustion of zirconium in oxygen. Coal combustion as well as reacting gas-particle flow is simulated in [34K].

16.3. Radiation and small particles

An increasing number of publications consider radiative heat transfer in systems involving small particles.

Hiers points out the importance of radiation in small particle combustion [41K]. Sazhin et al. [44K] study radiative exchange between a gas and fuel droplets. Dombrovsky [39K] models the radiative transfer from a small particle to ambient water through a vapor layer and the thermal radiation from non-isothermal particles of semi-transparent material [40K]. The influence of optical constants and particle size on the radiative properties and heat transfer involving ash clouds and deposits is considered in [36K]. Unsteady heat transfer in dilute suspensions of small particles is studied by Coimbra and Rangel [38K].

Lee et al. [42K] point out the importance of radiative transfer in thermophoretic particle deposition. Radiative and convective transfer through pneumatic transport of particles is studied in [35K]. Radiation and fluid-particle flow past a surface in the presence of gravity is studied in [37K]. Two-phase mixtures of non-gray gases with particles are considered in [45K]. The effect of thermal radiation on the sound wave propagation in gas-particle media is investigated by Park and Baek [43K].

16.4. Participating media

Papers in this category focus on emission and absorption properties, as well as scattering properties of the participating medium.

Several papers deal with the molecular emission and absorption properties. Vitkin et al. [62K] present an engineering procedure for calculating the transfer in molecular gases geared towards combustion of hydrocarbon fuels. Liu et al. [56K] present a statistical narrow-band correlated- k method to study 1- and 3-D enclosures containing CO_2 - H_2O - N_2 mixtures. The same authors consider band lumping strategies in [55K]. Kanne et al. [51K] study thermochemical relaxation through collisions and radiation.

Anisotropic scattering is involved in the radiative transfer in non-gray CO_2 containing carbon particles, as is discussed in [50K]. A model to evaluate the total emissivity of an isothermal, gray, anisotropically scattering particle-gas mixture is presented in [58K]. The influence of anisotropically scattering media is also subject of the studies by Nunes et al. [57K] of arbitrarily shaped, axisymmetric enclosures, and by Krishnaprakas et al. [53K] of boundary layer flow of a fluid. An integral equation formulation for transient transfer is reported in [64K], a new angular discretization scheme for 3-D radiative transfer with anisotropic scattering in [52K]. Media with isotropic scattering are considered in the study of Byun et al. [47K], and Zhou et al. [66K]. The YIX method and pseudoadaptive angular quadrature is used for ray effect mitigation in scattering media by Tan et al. [60K].

Le Dez et al. [54K] and Anteby and Arbel [46K] study radiative-conduction coupling in semi-transparent

media. Viskanta and co-workers discuss transient radiative heating of opaque and semi-transparent materials in [61K], and radiative transfer in semi-transparent glass foam blankets in [48K,49K]. Coupled radiation and conduction in absorbing and scattering composite layers is considered by Tan and co-workers in [59K,63K]. Yamada and Kurosaki [65K] investigate the radiative characteristics of fibers with a large size parameter.

16.5. Combined heat transfer

Papers in this subcategory consider the combined effect of radiation with conduction and/or convection. This year only few papers focus on combinations of conduction and radiation. Similarity solutions for collapsing cylindrical shock waves in radiating and conducting gas are presented by Hirschler and Gretler [73K]. Kiwan and Al-Nimr [75K] investigate the effect of radiative losses on a two-step parabolic conduction model. Shiff simulate radiation and conduction in a cylindrical volume [88K]. A spherically inhomogeneous medium is studied in [69K]. Conduction and radiation also dominate the operation of electric IR heaters studied by Petterson and Stenstrom [80K,81K]. Conduction/radiation in high-porosity fiber insulation is investigated in [76K].

A considerable number of papers discuss radiation combined with convection. Combined radiative heat transfer and natural convection are considered for an L-shaped corner [82K], for staggered and aligned arrays of nuclear fuel rods in rectangular enclosures [90K], for an air channel of LMR decay heat removal [89K], and for longitudinal fins [83K]. Han and Baek consider natural convection and radiation in rectangular enclosures divided by two partitions [72K]. Monnier uses finite element analysis to study free convection and radiation of gray bodies [77K]. Cheng et al. [68K] investigate the contaminant cooling by natural convection-radiation after severe nuclear accidents. Airflow, radiation and moisture transport also play an important role in heat release from the human body [78K]. Effects of radiation and thermal buoyancy on hydromagnetic flow are considered by Chamkha [67K]. Combined radiation and forced convection are studied for helical pipes [92K] and for flow of micro-polar fluids over a horizontal plate [70K]. The combination of radiation and forced convection also plays a role in low-pressure chemical vapor deposition [79K], and physical vapor deposition [87K]. Convection/radiation is also dominant in arc heaters [74K], and the X-33 linear aerospike plume-induced base heating [91K].

All three heat transfer modes are studied by Roy et al. [86K] in a silicon tube growth system, and by Ergin [71K] in surface radiation in two-floor enclosures. Rousse and co-workers [84K,85K] present a control

volume finite element method to study 2-D problems involving all three heat transfer modes.

16.6. Intensely irradiated materials

Several papers deal with materials intensely irradiated by laser radiation or microwaves. Energy transfer and plasma formation under laser irradiation were studied by Gusíkov et al. [94K]. Stable and critical regimes in the laser heating of carbon particles are discussed in [96K]. Pfefer et al. [98K] use a YAG laser to investigate photocoagulation of albumen. The temperature response of an absorbing and scattering medium to laser irradiation is investigated by Tan et al. [100K]. Guo et al. [93K] report Monte Carlo simulations of short-pulse laser transport. Micro-wave sintering is studied in [97K]. A simulation of micro-wave and conventional ovens as well as hybrid ovens is reported by Haala and Wiesbeck [95K]. Samaras et al. [99K] present heat transfer computations for non-ionizing radiation in biological tissue.

16.7. Experimental methods

Only few studies of experimental methods are reported this year. Bertrand et al. [101K] report pyrometry applications in thermal plasma processing. Surface brightness measurements from satellites offer the possibility of mapping surface heat fluxes. Norman et al. [104K] present a dual temperature-difference method to minimize measurement errors. The transient temperature behavior of multistage cryogenic radiators is studied in [102K]. Hatchard et al. [103K] study the importance of radiative heat transfer in Li-ion batteries during thermal abuse.

17. Numerical methods

Simulation of fluid flow and heat transfer by numerical techniques has by now become a significant part of fundamental research and practical applications. Research continues in the development of improved techniques for heat conduction, convection and diffusion, phase change, radiation, and fluid flow. In this review, the papers that primarily describe the *application* of numerical techniques to specific physical problems are included in the appropriate application category. The papers that describe the development of numerical methods are reviewed in this section.

17.1. Heat conduction

A domain decomposition technique is used for solving 3-D finite-difference equations for heat conduction [3N]. The technique is further extended to a hybrid method involving finite-element and finite-difference

formulations [4N]. Cheng and Wu [2N] describes a combination of grid-generation and conjugate-gradient methods for shape design.

Inverse heat conduction problems have received considerable attention. An approximate inverse has been applied to a 1-D problem [6N]. Two-dimensional nonlinear inverse problems have been solved by finite-element techniques [7N]. The inverse method is used to estimate fluid temperatures within an instrumented probe [1N]. Maciag and Al-Khatib [8N] investigates the stability of over-determined inverse problems. Laplace transforms are used to solve an inverse problem [9N]. A novel inverse methodology is used to estimate time-dependent heat flux [10N]. A 2-D inverse problem is solved to determine the unknown thermal conductivity [5N].

17.2. Convection and diffusion

A 2-D scheme is developed for convection and diffusion with linear production [11N]. A higher-order characteristics upwind method is described for unstructured grids [12N].

17.3. Phase change

A formulation based on the Second Law is applied for solid–liquid phase change [16N]. A fast and accurate way for solving phase-change problems is described [17N]. A network approach is proposed for modeling solidification in complex geometries [18N]. A moving-boundary method is used for the calculation of droplet spreading and solidification [19N]. Domain decomposition methods are applied to the aluminum casting process [15N]. A fixed grid finite-difference method is described for phase-change problems [14N]. An adaptive scheme is proposed for situations involving solid–liquid phase change [13N].

17.4. Radiation

An inverse radiation problem is solved using a conjugate-gradient method [22N]. A finite-volume scheme is presented for radiative heat transfer in semi-transparent media [21N]. Chai and Moder [20N] describes an angular-multiblock procedure for radiation.

17.5. Fluid flow

The SIMPLE algorithm and its variants for the solution of flow equations were originally introduced for a staggered grid. A number of papers describe extensions of the method for non-staggered or colocated grids. A method is presented for curvilinear non-staggered grid [33N]. An improved SIMPLE algorithm is described for a colocated grid [32N]. A pressure-based algorithm for non-staggered grids is applied to incompressible flows

[24N]. A colocated-grid, fully coupled algorithm is used for large eddy simulation of incompressible and compressible flows [23N]. A non-staggered, curvilinear-coordinate method is developed for free-surface flows [30N].

A unified formulation is described for SIMPLE-like segregated algorithms [29N]. A method is proposed for an automatic determination of relaxation factors for the SIMPLE algorithm [28N]. A SIMPLE-like conservative method is used for a transient flow [31N]. A new block-implicit method is reported for flow in rectangular enclosures [25N]. A numerical scheme based on Fourier expansions is presented for a 3-D flow [36N]. A treatment is described for flow problems with specified pressure boundary conditions [27N]. A 3-D *diagonal* Cartesian method is applied to complex geometries [26N]. A vorticity-stream function formulation is used for natural convection [35N]. A meshless method for laminar natural convection is evaluated [34N].

17.6. Other studies

The Second Law is used to impose a time-step constraint in transient calculations [37N]. A procedure is described for maintaining the heat-flux continuity in conjugate heat transfer problems [38N]. A boundary-domain integral method is used for conjugate heat transfer [40N].

A conservative flux-splitting technique is applied to multi-component flows [42N]. The volume of fluid (VOF) technique is extended to spherical coordinates [41N]. A higher-order upwind scheme is used to calculate wave propagation based on a hyperbolic two-fluid model [39N].

18. Properties

Experimental measurements of thermal conductivity for a host of systems, simple and complex, by a wide variety of methods distinguished the research in this section.

18.1. Thermal conductivity and diffusivity

For simple systems, results of experiments are reported for; Binary beryllium beds used in next generation fusion reactors, isotope effects on boron carbide diffusivity; monolithic carbon thermophysical properties; heat transport in He-3 below and above convection onset in a Rayleigh–Benard cell; parahydrogen–ortho-deuterium solid solutions with varying concentrations (0.01–100%) of the latter; CH₄–Kr solid solutions with varying concentrations of the former (0.2–5%) at temperatures 1.8–40 K; NbTi superconducting wire and the influence of wire coatings; solid SF₆ in the high-temperature phase; for tetragonal zirconia ceramic

hemispherical total emissivity determinations from spectral analysis yields thermal conductivity data [3P,7P–9P,15P,18P,25P,31P,33P]. For more complex and practical systems further experiments provide data on: coal ash and synthetic ash samples: the relationship between effective conductivity of an evacuated powder and bulk conductivity of the same material; insulating properties for perpendicular-laid versus cross-laid lofty non-woven fabrics; rigid polyurethane foams blown with different hydrocarbons: nanosystems electron dynamics, suspension of nanophase powders in a base liquid and a novel temperature jump apparatus for observing transient temperature; Kapton HN between 0.5 and 5 K [4P,13P, 17P,22P,24P,26P,37P,38P,40P]. Suspensions in shear flow fields are studied, Bi-2223/Ag/barrier/Ag tapes with various oxide barrier materials evaluated, and the coupled heat and mass transfer in soils and mulches considered [11P,16P,29P,30P,36P]. With emphasis upon the experimental technique results are given for: Diffusivity in disk-shaped samples (graphite and boron nitride); hemispherical total emissivity (Vycor and fused silica glasses); emission spectroscopy (soot particle determination in ethane diffusion flames); in situ high-temperature conductivity measurement (impurity concentration on boiling surface crevice or a steam-generator element); flash method (effect of thin layer on diffusivity measurement) [14P,21P,23P,28P,32P].

Models are devised for a number of heat and mass transfer phenomena: The drying process of an anisotropic biological product (sweet potato); the period of crystal growth during frost formation; predicting the thermal performance of complex aerospace structures; cooling systems designed for optimum conditions including energy savings and quality of product; predictive models tested against conductivity data for soil samples at high temperatures (30, 50 and 70 °C); conductance of thin layers with randomly oriented composites using percolation theory [1P,5P,10P,19P,27P,34P]. Other analytical approaches are taken to study a number of problems: the conductivity, cellular structure and matrix polymer morphology of an assembly of chemically crosslinked, low density, closed cell polyolefin foams; spatially dependent conductivity (K_x) of heterogeneous materials; soil conductivity at very low moisture content and moderate temperatures; transient thermal behavior of composite material; determining temperature dependent properties from temperature responses measured at medium's boundaries; using an artificial neural network to determine conductivity detection response factors; conductivity of I-D Fibonacci quasi-crystals [2P,6P,12P, 20P,35P,39P,41P].

18.2. Diffusion

The few papers in this area are concerned with: the determination of the diffusion coefficient–vapor pressure

product for 11 liquids from hanging drop evaporation measurements; irreversible thermal–diffusional coupling in local equilibrium; estimating the diffusion coefficient of tungsten and carbon introduced in liquid cobalt through the dissolution of tungsten carbide; the classical diffusion model of vibrational predissociation of van der Waals complexes [42P–45P].

18.3. Viscosity

Limited work in this area observe: the influence of fluid properties on electrohydrodynamic heat transfer in liquids under viscous and electrically dominated flow conditions; apparent molar volumes and viscosities of DL- α -alanine in water–ethanol mixtures; the crystallization fraction under shear using the shear flow rheometer (SFTR); the break temperatures of mould fluxes in continuous casting for steady-state and dynamic measurement of the viscosity. Viscosities for solutions of glycine, alanine, butyric acid, valine, leucine and serine aqueous urea have been calculated at four temperatures about 300 K [46P–50P].

18.4. Transport properties

A pulse method is used to measure thermal conductivity, specific heat capacity and thermal diffusivity of polycrystalline ZnIn_2Se_4 in the 300–600 K range. Analytical works describe: an improved dynamic molecular collision (DMC) model particularly suited for calculating viscosity and thermal conductivity values in rarefied gas flow; transport coefficient in non-equilibrium diatomic gas flow; simple methods for estimating diffusion, viscosity and thermal diffusion from collision integrals for a gas composed of carbon and nitrogen atoms [51P–54P].

18.5. Specific heat

Experimental works consider the role of system thermal conductivity when temperature modulate differential scanning calorimeter (DSC) is applied to measure specific heats of materials; a micro-calorimeter is employed to measure partial molar heat capacities of some saccharides in aqueous urea solutions; adiabatic vacuum calorimetry yields temperature-dependent heat capacities for hydrofullerene, $\text{C}_{60}\text{H}_{36}$; a calorimeter and densimeter are combined to measure heat capacities and densities of liquids and liquids with dissolved gas; optical dump probe spectroscopy measurements show the influence of the magnetic specific heat; for copper–tin (Cu–Sn) alloys rapid solidification experiments and cooling curves permit specific heats to be evaluated. An analysis indicates the impact of variable fluid heat capacities upon the performance of adsorption refrigeration cycles [55P–62P].

18.6. Thermodynamic properties

Differential scanning calorimetry is used to study isothermal curing of a thermosetting system, yielding data on reaction rate and heat transfer. Analytical investigations examine enthalpy, temperature and quality of non-azeotropic refrigerant mixtures in the phase-change region; the behavior of unsaturated moist air as given by the systems thermodynamic functions and their derivatives; a model of liquid crystalline polymer (LCP) fibers material during the manufacturing process; the influence of multipolar and induction interactions on the speed of sound; a mathematical model for computing thermodynamic properties in the liquid, gas, and two-phase domains using statistical thermodynamics; the thermodynamic properties of alternative fluid pairs for absorption thermal systems [63P–69P].

18.7. Miscellaneous

Experimental property data are reported for the following systems: soot-optical properties when produced from acetylene and ethene flames; a new segregated fluoroether with a global warming potential < 3% of comparable perfluorocarbon fluids and superior heat transfer performance; cubic majorite (one of the primary components of earth's transition zone) – bulk modulus; Inconel 718 – total hemispherical emissivities; metal and composite structural materials in aerospace applications – effect of surface heating on reflectance. A numerical heat transfer model predicts temperature profiles during high-pressure thawing [70P–74P].

19. Heat transfer applications – heat exchangers and heat pipes

Efforts center on enhancing heat transfer, fouling and other aspects of exchanger surfaces, mathematical modeling and analysis and factors affecting performance.

19.1. Compact heat exchangers

A group of papers gives the results of experiments for: an absorption heat transformer using the mixture TFE-E181, louvered fin-and-tube exchangers in wet conditions, evaporative heat transfer for R-22 and R-407C-oil mixture in a microfin tube with U-bend, heat transfer and pressure drop of R-22 in smooth/micro-fin tubes and heat exchange for compact plate exchangers used as evaporators and condensers in refrigeration loops [1Q–5Q].

19.2. Design

Heat exchangers can play a crucial role in avoiding pollution worldwide by an industrial design process

which incorporates their use at the outset. Two shell-and-tube exchangers, physically alike in every respect, are compared for different flow configurations (regular versus chaotic advection flow) at Reynolds numbers from 30 to 30 000. Charts are derived to determine approximate area requirements for exchangers using plain and low-finned tube bundles. Other works show that: the main architecture of counterflow exchangers can be determined by thermodynamic optimization with volume constraint; computational fluid dynamics (CFD) numerical models are useful in the design or refit of pulverized coal – fired boilers; design of heat exchangers can strongly affect final heat exchanger network (HEN) synthesis; exchanger design influences system performance of silica gel absorption refrigeration systems and the heat transfer and flow characteristics of slit fin exchangers [6Q–14Q].

19.3. Enhancement

A host of papers describes the efficacy of various means of enhancing heat transfer. Thus thirty-six exchanger (12 plate-fin, 12 wavy-fin and 12 louvered-fin) geometries were tested for heat transfer and pressure drop characteristics. The carbon steel spirally fluted tube in investigated as a replacement for the smooth copper tube normally used in high-pressure preheaters of power plants. Airside performance of fin (and superslit fin)-and-tube exchangers with plain fin configurations is determined by testing 18 samples. Other investigations consider the use of acoustic resonant standing wave fields, an anionic surfactant, the effect of a single oblique pin fin on endwall heat transfer, and a new tube – the inside and outside spirally triangle finned tube (10STF Tube). Experiments also include work on special systems or conditions: wavy fin-and-tube exchangers under dehumidifying conditions, finned water wall tube in fluidized bed boiler, inserts for a recuperator, annular finned pyrolyser, spray towers with and without fin coils, and condensate carryover in dehumidifying, finned tube exchangers [15Q,16Q,19Q,20Q,22Q–25Q,27Q,30Q,33Q–35Q,37Q].

Analytical efforts include correlations, visualization and numerical computation, comparisons of mathematical models and the assessment of specific enhancement designs. Correlations are given for heat transfer and friction characteristics of plain fin-and-tube exchangers, generalized friction effects for louver fin geometry, and airside data for plain fin-and-tube exchangers in wet conditions. Flow visualization and numerical computation examine the influence of fin spacing on the over-tube side of a single row fin tube exchanger. Three different mathematical modes are compared for their ability to account for the augmented heat transfer of in-tube flows in the presence of an array of equally spaced plate fins attached at the outer surface.

Other efforts consider vortex generators (delta winglet pairs) for plate-fin heat transfer enhancement, a model for condensation heat transfer on a horizontal finned tube with non-condensable gases present, enhancement and heat exchanger network retrofit, performance assessment, and a survey of recent fin-and-tube exchanger patents [17Q,18Q,21Q,26Q,28Q,29Q,31Q,32Q,36Q,38Q].

19.4. Fouling and surface effects

Efforts continue to understand, control and prevent the fouling of heat transfer surfaces. These efforts include: the influence of surface energy and surface roughness on calcium sulphate deposition, the use of paint protection to control corrosion and fouling of thermosiphon economizer tubes, long-term fouling tests of cooling tower water flowing in enhanced tubes to determine the mechanism of fouling, and the effect or operating parameters on the deposition of calcium sulphate and calcium carbonate mixtures – the most common constituents of heat transfer surface scale. Other works treat: thermal resistance measurement of porous deposits under single-phase forced convection and flow-boiling conditions, the fouling of two types of copper-modified surfaces of low surface energy, the fouling of alloy-800 surfaces by magnetic particles, and the use of an organic monolayer coating to promote dropwise condensation. Preventive and cleaning approaches involve novel biological inhibitors developed by protein and genetic engineering, the use of the antiscalant polyphosphonate, relative merits of four scale-removal methods, and enhanced cleaning of whey protein soils using pulsed flows [39Q–42Q,47Q–50Q,52Q,59Q,61Q–63Q].

A comparable analytical and mathematical modeling effort addresses fouling and related matters of economics, optimal cleaning programs and thermodynamic performance. A new composite model is proposed for CaSO_4 fouling which accounts for both crystallization and particulate fouling and predicts fouling resistance during cleaning and fouling cycles. A mathematical model for initial chemical reaction fouling is tested and a new strategy described for mitigating exchanger fouling by modifying molecular interactions at the interface between heat transfer surface and the/adjacent deposit. A cost model is proposed linking maintenance and thermal performance of exchangers, a related work uses entropy generation to represent the effect of fouling and a third effort gives a probabilistic approach to represent fouling models in common use. Heat exchanger networks (HENs) are involved with scheduling short-term cleaning, retrofitted using pinch analysis, and a dynamic neural network control models predictive control strategy. Concluding works describe a fault diagnosis method for early detection of fouling and review composite fouling

of aqueous exchangers [43Q–46Q,51Q,53Q–58Q,60Q,64Q].

19.5. Mathematical modeling/analysis

The scope of work in this section embraces condensers, evaporators, a variety of heat exchangers, exchanger networks, control, and regenerators. The emergency condenser of an innovative boiling water reactor (BWR) is simulated; the divided condenser of a molecular evaporator modeled and the geometrical and operating parameters for evaporative coolers optimized. Parallel-plate, double flow and counterflow double-pass exchangers, created by inserting an insulated or impermeable sheet, are analyzed. Other works consider: a lumped parameter model of operating limits of a one-wall geothermal plant exchanger; parallel-flow exchangers with ambient interaction; heat and mass transfer for parallel air flow and falling desiccant film; comparison of 1- and 2-D models for wet-surface fin efficiency in a plate-fin-tube exchanger; a “gray box” model for exchanger fault detection and diagnosis; and the modeling of the controlled atmosphere brazing (CAB) process for automotive aluminum radiation manufacturing. A new nonlinear model for exchanger network retrofit considers the distribution of heat transfer area and pressure drop and the robustness of fuzzy control as applied to a thermal plant is described. Regenerators are the focus of works: solving the set of partial differential equations which physically model blast furnace stoves, using Second Law exergy analysis, linking heat transfer to pressure drop, to assess performance, and analyzing transient behavior of a regenerator bed using a hyperbolic dispersion model [65Q–80Q].

19.6. Performance-factors affecting

A number of works approaches exchanger performance from the Second Law of thermodynamics. A cross-flow plate heat exchanger with unmixed fluids, analyzed for balanced flow, identifies the exchanger characteristics which determine the minimum entropy generation number. A wet cross-flow exchanger operating at various weather conditions is examined from Second Law principles and the concept of an isentropic heat exchanger with regenerative work transfer is developed. Following a review of various second law approaches, a rational method is presented which satisfies physical requirements. Low temperature condensation data are given for hydrogen with various exchanger geometries and the energy transfer mechanisms at the solid/liquid interface between liquid He-3 and Ag sinter heat exchangers. Disuniformities of fluid properties and maldistributions are considered for their effect on condenser and evaporator performance. Experimental data for a single circuit, multi-pass heat exchanger,

typical of an element of a packaged air conditioning unit, validates a cross-flow exchanger program (ACOL5) for air conditioning applications. A standard methodology is recommended for data reduction, when obtaining air-side performance of fin-and-tube exchangers, which should improve the development of correlations or performance comparisons [81Q–93Q].

19.7. Power and reversed cycles

Experimental results are reported for several systems: low- and high-temperature performance of a single stage superfluid stirling refrigerator (SSR) using a plastic recuperator; performance of a heat pump system using hydrocarbon refrigerants (single component – propane, isobutane, butane and propylene and binary mixtures – propane/isobutane and propane/butane); and existing data utilized to correlate performance impacts attributable to liquid – suction exchangers of refrigeration systems. Analytical and numerical works range over a number of systems as well: the rotary system for continuous cooling by solid–gas sorption is modeled by counter-flow heat exchangers in series; a numerical model proposed to investigate the performance of air-cooled condensed coils; the effect of oscillating flow of gap fluid on shuttle heat transfer in reciprocating expanders analyzed; the generator performance of a lithium bromide – water vapor absorption chiller estimated; the performance of liquid desiccant cooling systems simulated to facilitate the development of energy efficient alternatives to conventional air conditioning practices; and the orifice pulse tube refrigeration modeled, showing an association of refrigeration load and entropy flow [94Q–102Q].

19.8. Shell and tube/plate heat exchangers

For shell-and-tube exchangers an algorithm provides a cost comparison between an optimized, enhanced tube heat exchanger and one with optimized plain tubes. A physically based model is developed to predict void fractions for upward cross-flow through horizontal tube bundles in good agreement with measurements for R-11 and air–water mixtures. Turbulence-induced tube vibrations due to baffle plates with flow hole nozzles is reported and an editorial promise that “real-world experiences” will be regularly published for practicing heat transfer engineers. For plate exchangers, observations of nucleate and convective boiling (of CFC114) in plate fin units are reported and heat and fluid flow in corrugated-undulated plate devices investigated. Analytical efforts consider: the hydrodynamical and thermal character of corrugated channels using computational fluid dynamics; the transient response of multi-pass exchangers based on axial heat dispersion with deviation from ideal plug flow accounted for; the numerical investigation of

2-D forced convection heat transfer over a plate with protruded transverse groove fins; a general calculation method which allows a determination of temperature profiles simulation of wall heat flux and dispersion in exchanger passages; and the investigation of falling film and bubble types of the ammonia–water absorption process [103Q–113Q].

19.9. *Thermosyphons/heat pipes*

Micro and miniature heat pipes and the novel application of heat pipes distinguish the papers of this section. Three coupled models (for the micro-region, 2-D wall conduction and longitudinal capillary two-phase flow) predict 3-D steady-state in a micro-heat pipe array. Thermosyphons employing enhanced structures offer an alternative to liquid immersion and are suitable for point cooling applications as very compact evaporators. The radially rotating, miniature, high-temperature heat pipe is wickless; its performance is analyzed by appropriate flow and heat transfer models and experimentally tested. Flat miniature heat pipes are optimized using existing and new data and quasi-Newton algorithms.

The performance of conventional gravity assisted heat pipes and modified heat pipes with a separator in the adiabatic section is investigated experimentally, as is the performance of a flat-plate heat pipe. Analytical studies consider: thermal transients in a capillary evaporator prior to boiling initiation; transient characterization of flat-plate heat pipes during startup and shutdown phases; the effect of dimensionless parameters on heat transfer characteristics of an inclined, closed, two-phase thermosyphon at normal operating conditions; and a unique thermosyphon condenser designed to utilize drainage disks in the condenser to improve heat transfer. Several papers report special recent application of heat pipes: the capillary pumped loop (CPL) for cooling spacecraft and telecommunication devices, incorporation of heat pipes in a latent heat storage unit used in the low energy cooling of buildings, waste heat recovery using heat-pipe heat exchanger (HPHE) in hospital surgery rooms, and the application of miniature heat pipes for mobile PC cooling systems [114Q–127Q].

19.10. *Miscellaneous*

Scraped surface heat exchangers are investigated for electrodiffusional wall shear rate, temperature heterogeneities at exchanger outlet and residence time distribution modeling (RTD) of food product by a neuro-computing approach. The rapid cooling of hot foods is studied using various high-heat transfer rate devices. Evaporation rate of an electron-beam evaporator is modeled allowing for interaction effects between the beam and the evaporant. In an industrial environ-

ment an adaptive, nonlinear control method is successfully applied. A series of papers describes efforts to improve the energy efficiency and environmental quality of industrial and commercial processes: energy saving and pollution control in ultra high-power electric-arc furnaces, recirculating fluidized bed (RCFB) incineration of solid, liquid, gaseous wastes – energy equations and performance, desiccant air conditioning systems incorporating rotary heat and mass exchangers, thermal behavior of closed wet cooling towers used with wet ceilings. Downflow tube-reactors have attracted attention for their ability to promote heat and mass transfer and accelerate high-temperature gas–solid reactions for fine powders. A brief review presents research progress on dropwise condensation heat transfer in China for the past decade [128Q–139Q].

20. Heat transfer – general applications

20.1. *Buildings*

Computers have become an indispensable tool for engineers having to predict energy histories of buildings and similar structures. Many contributions in the literature propose and describe how to perform energy balances by computer analysis for structures to be heated or cooled through ventilation or climatization. Paper [11S] suggests how to plan a heat transfer analysis effectively for multi-zone buildings. The prediction of velocities and temperatures in naturally ventilated buildings is discussed in [12S]. An experimental technique to determine heat transfer functions is based on a neural network [4S]. Turbulent flow is simulated [13S]. Paper [14S] presents a mathematical model that simulates local velocities and temperatures in 3-D building models for given meteorological conditions. Experiments and computer simulations are performed [10S] in residential applications for different insulation levels. The temperature rise in concrete nuts was measured under adiabatic conditions [9S]. The finite element formulation and the numerical strategy for the analysis of a telescope building is developed [6S]. The measured temperatures in a ground floor slab were simulated in [2S] and compared [1S]. The optimal distribution of thermal insulation of underground structures is minimized [5S]. Giaconia and Orioli [7S] describes how to calculate transfer function coefficients. The paper [3S] calculates fire growth in industrial cable arrays. The dispersion of vapor from an accidental fire is calculated [8S] for a building.

20.2. *Meteorology*

The energy budget of the ground surface and the air boundary layer above was measured [21S] in the wet

savanna. A paper [22S] explores the need for a more complex formulation of the vegetative energy balance. Sensible heat flux radiometric surface temperature measurement is discussed [24S]. An urban surface temperature model with turbulent heat fluxes is presented [27S]. The sensitivity of a regional climate model is improved by a reflective upper boundary condition [26S]. A numerical model of the hydrodynamic structure of an artificial lake was designed [16S]. Temperature anomalies and the decay of wave induced turbulence near the ocean surface was interpreted as a consequence of wave breaking. A paper [18S] discusses the mantle convection process. The temperature observations in the near surface layer of the ocean reveal brief fluctuations due to wave traveling [23S]. Simulation with the Miami Ocean Model (MICOM) explored its accuracy [29S]. The atmospheric response to spatial variations of the concentration in the Southern Ocean is discussed [20S]. The paper [17S] describes the thermal regime of retrogressive thaw in the Yukon Territory. A method to identify changes in the structure of a solid is based on heat transfer studies [31S] in Argentina. A 2-D model [30S] studies heat transport during the evolution of the Baikal rift. The sensible heat flux is estimated [28S] from the radiometric temperature over a crop canopy. Numerical models of transient fluid flow and heat transport are compared with and without buffering in basement rocks [25S] in the Arcoma foreland. Numerical simulation of coupled, thermal, hydraulic and mechanical behavior is validated [19S] by experiments and numerical simulation. A critical injection rate [15S] determines simulation of effectiveness parameters for laboratory scale simulation of steam injection in oil recovery.

20.3. Thermodynamics

The optimum thermodynamic match between two streams at different temperatures is determined by maximising the power generation associated solely with the stream to stream interaction [38S]. Three problems are considered in [37S]: (a) maximal work produced in a thermodynamic system in finite time; (b) minimal work to be done in order to transform an equilibrium system into a number of subsystems and (c) maximal power obtained in a finite time. Cogeneration of various energy forms in a single equipment depends on the thermodynamic parameters of the system [36S]. In a Lenoir cycle with regenerative heating, the entire positive work is available for external consumption [35S] since the negative work is supplied by the atmosphere. The optimal heating and cooling rates for the reversed Ericsson cycle with ideal regeneration is determined [33S] for heat pump operation. Ref. [34S] fluid dynamic analysis provides useful insight into heat transfer processes in electronic systems [32S].

20.4. Engines

A numerical simulation analyses the transient in a solid rocket ignition process [40S]. The $k-\epsilon$ model with a wall function describes wall turbulence. Transient heat transfer and water condensation in the engine exhaust system influence the conversion of carbon monoxide, hydrocarbons, and nitrogen oxides in the convertor of an engine in cold start [39S]. Local convective heat transfer is started from a coaxial rotor to the crown shaped stator experimentally [41S]. The results of flow visualisation in turbomachinery are discussed [42S]. A new turbulent flow system consisting of a cruciform burner with two cylindrical vessels is proposed [43S]. A 3-D finite element heat conduction code was developed to calculate the temperature distribution in the three piston head and cylinder liner of a heavy duty diesel engine [44S].

20.5. Nuclear reactors

A thermal mockup of a simulated CANDU 3T bundle within a fuel basket was studied experimentally [45S] to obtain fuel rod temperatures. An analytical model computed the two 2-D velocity profile of the hot fuel elements of a pressurized water reactor core [51S] following a break and loss of coolant. The pyrolysis of *n*-butane initiated by methyl radicals was studied in the temperature range 750–1000 K in a quasi-wall-free reactor [46S]. Corrosion products in the secondary system of a pressurized water reactor accumulated in the steam generator in regions of stagnant flow. The paper [50S] describes such a sludge collector. Experimental information was obtained [49S] on the temperature of fuel elements in the transcritical region. Sodium experiments on a scram transient experiment [47S] clarified flow and heat transfer in a fast reactor core under natural circulation conditions. The use of large scale storage systems for spent fuel is considered in Japan. The present experiment [48S] studies the heat removal from the vault storage system with passive cooling in a 1/5 scale model. The Richardson number appears to be the most representative parameter.

20.6. Chemical reactors

Radial velocities due to temperature gradients are calculated [53S] inside a continuous annular Chromatograph Simulation software. Modern hydrocarbon absorbers are promising candidates [64S] for cold start emission control of gasoline engines. A model of a charring heat shielding material is used [66S] to investigate heat and mass transfer at high temperature. A paper considers the extraction of power from a stream of hot gas [77S]. The vapor deposition process of silicon is modeled [55S] numerically. A 3-D model [76S] predicts

the temperature distribution in a proton membrane fuel cell. Data are presented on hydride storage for a fuel cell [67S]. The integration of a steam reformer in a fuel cell is examined. Closed form expressions are derived [58S] for the bulk mean and the catalyst temperature of a catalytic converter. The velocity vectors and the strain rate distribution were measured [71S] for the first time in a baffled column. The film blowing process was numerically simulated [74S]. The heat transfer coefficient in a helical agitator was calculated [75S] based on experimental data. Chemical vapor deposition of crystalline diamond films is studied [59S]. Chemical deposition of a thin film on a moving surface is numerically investigated [54S]. The Maxwell–Stefan method with proper approximations was used to model mass transfer in distillation columns [52S]. Another model for the design of distillation columns is imported [81S]. The vapor deposition in a horizontal chemical reactor is analyzed based on the basic 3D flow, heat, mass transfer equations [72S]. The same equations are used [56S] to optimise a vapor deposition reactor. Chemical deposition in free molecular gas flow through cylindrical channels is analyzed [62S]. Fast drying can reduce granulation time by half [69S]. An increased utilization of biomass for heat and power production can reduce emissions of CO₂ [78S]. The heat transfer coefficient is found experimentally to increase in a cyclone separator with circulation rate and as velocity [60S]. The operating parameters of tubular coking heaters can be predicted by mathematical modeling [79S]. A reformer model for a molten carbonate fuel cell [61S]. A mathematical model simulates the temperature in molten carbonate fuel cells [63S]. A novel moving and stirred bed reactor achieves thermal decomposition of tyre particles in vacuum [80S]. A general model simulates a sludge reactor operational for dispersive flow [68S]. The hot blast stoves at the Ispatt steel facility in Chicago are controlled based on a dynamic model [70S]. The pyrolysis of coal in a furnace is modeled [73S]. Numerical methods describing combustion kinetics in coal fixed boilers is described [57S]. Frontiers in refrigeration and cooling at very low temperatures are discussed [65S].

20.7. Manufacturing and processing

The thermal storage characteristics of aluminium plates are discussed under heating in electrical and natural gas furnaces [112S]. A method for the simulation of temperature stabilisation in tools during multi-cycle cold-forging operations combines thermo-mechanical plastic simulation and heat transfer [109S]. A model calculates interphase pressure in order to predict the heat transfer in spot welding [95S]. A model [100S] calculates heat transfer in down grinding. The transient slab temperature distribution in the reheating furnace for rolling of steel slabs is predicted [97S]. Calculations

and local temperature measurements determine [89S] thermal crowning in work rolls left in air to cool. The effect of scaling and emulsion delivery on heat transfer during hot rolling of steel strips is examined [111S]. The surface heat transfer coefficient and the appearance of the surface of the strip depend on process variables [103S]. Rapid thermal processing has become a key technology in the fabrication of advanced semiconductor devices [104S]. A paper [92S] describes the computer simulation of the deep narrow extrusion of a thin-walled cup. Deformation and temperature are simulated for hot backward extrusion by an elastic and rigid-plastic finite element method [91S]. Steady state 3-D analysis studies [102S] 3-D extrusion using automatic mesh generation.

The simulation of heat transfer and cure in pultrusion predicts these processes well [105S]. A heat transfer model coupled with an optimization scheme is presented in [84S]. A finite element analysis [110S] is supported by temperature measurements with embedded thermocouples. A computational scheme determines optimal conditions and geometry for a continuous quenching process [85S]. The internal structure of steel bars after treatment with the Temcore method are predicted mathematically [83S]. Minimills are introducing mould powder as lubricant for the continuous casting of steel billets. An experimental study [108S] investigates this. The location of the phase-change interface and the temperature field are calculated for a continuous casting process [88S]. Experiments study hot dip coating of steel with Al–Zn–Si alloy [87S]. The Kirchoff transformation is used to simplify the equation describing the heat transfer in continuous casting of steel [90S]. A 3-D model simulates the die-casting process [94S].

Heat transfer in the weld pool and work piece are studied in arc and beam welding [106S]. Analysis describes heat flux in multiple pass welding [113S]. The methods described above are also used for the study of manufacturing processes of polymers [82S,86S,93S,96S,98S,99S,101S,107S,114S].

20.8. Food processing

Baking conditions were observed for two multi-zone industrial ovens temperatures, air velocities, and humidity were measured [115S]. The coupling between electromagnetics and heat transfer were studied through changes in dielectric processes during heat transfer [125S]. Application of process engineering methods have recently improved the understanding of the principles in deep-fat frying. The heat transfer coefficient in steam retort processing was measured [124S].

A neural network was used to predict temperature, moisture, and fat transfer in foods coated with edible films [123S]. A neural network was developed to predict temperature and moisture during thermal processing of frankfurters [119S]. Temperatures predicted by a 2-D

model were in good agreement with measured values [118S]. The numerical model provided a useful tool to evaluate batch high-pressure processes of foods [117S].

Heat and mass transfer processes in cold storage of food and vegetables are studied [116S] and natural losses are measured [121S,122S]. The temperature rise in packaged frozen food is modelled numerically in the distribution chain [120S].

21. Solar energy

Papers are broadly divided into solar radiation, low-temperature solar applications, building applications, and high-temperature solar applications. Papers on solar energy or energy conservation that do not focus on heat transfer, for example, papers on photovoltaics (except for those that deal with building integrated components), wind energy, architectural aspects of building design, and control of space heating or cooling systems are not included.

Papers that do not fit into one of the technology areas include an overview of the US Department of Energy's Office of Solar Energy Technologies [2T], an analysis of solar energy technologies from an environmental standpoint [3T], and an evaluation of renewable options to generate electricity [1T].

21.1. Radiation

The purpose and status of the US SURFACE RADIATION budget observing network (SURFRAD) established in 1995 to support satellite retrieval validation, and climate, hydrology and weather research is described in [4T].

Several papers analyze and interpret data for specific sites. Craggs et al. [5T] look at the effect of the duration over which averages of solar irradiance are computed on the short-term prediction of solar irradiance of an urban site in the UK. Jacovides et al. [8T] use spectroradiometric measurements taken in Athens in 1995 to investigate the influence of gaseous pollutant and aerosols on the spectral radiant energy distribution. Utrials et al. [19T] compare spectral values of the aerosol optical thickness measured in Valencia, Spain from 1993 to 1997 to boundary layer aerosol models in ZD-LOA and LOWTRAN7. Udo [18T] uses clearness index and relative sunshine to characterize sky conditions in Nigeria. He recommends an empirical expression relating monthly maximum clearness index and monthly average clearness index for tropical locations. Soler [16T] expresses zenith luminance for cloudless skies in Madrid as a function of solar elevation. Pereira et al. [10T] show that models based on clear skies overestimate incoming solar radiation in Brazil by as much as 44%. The discrepancy is attributed to burning of biomass. The

aerosol radiative forcing and stratospheric temperature response of the Mount Pinatubo volcanic eruption are evaluated using updated spectral optical property data in [11T]. Global and diffuse radiation pyranometer measurements in a Mediterranean location are used to investigate the diurnal and seasonal variations of atmospheric turbidity using Linke's factor [12T]. Ianetz et al. [7T] present a statistical analysis of global and beam radiation to compare the suitability of sites in Israel for utilization of solar energy.

Many papers present new or modified modeling approaches to evaluate measured data. [6T] discusses two new models to predict monthly average hourly global irradiation distribution from daily values. A quadratic in the sine of solar elevation is found to fit measured data well at 135 locations. A clear sky model developed in the framework of the new digital European Solar Radiation Atlas (ESRA) is compared favorably to other models and ground measurements [13T]. Sfetsos and Coonick [15T] introduce a new artificial intelligence based method for forecasting mean hourly global solar radiation on a horizontal surface. Mohandes et al. [9T] use radial basis functions to estimate monthly mean daily radiation on horizontal surfaces. Sen [14T] presents a solar irradiance polygon concept for evaluating variations of monthly, seasonal and annual global irradiation. Suehrcke [17T] presents a relationship between the duration of sunshine and solar radiation on the earth surface. The relationship is derived from monthly average values of daily beam radiation which are used as a measure of the fraction of clear sky. The relationship is validated for sites in Australia and is suggested to be universally applicable.

21.2. Low-temperature applications

Low-temperature solar applications include domestic water heating, space heating and cooling, desalination of water, cooking, waste treatment and solar ponds. Within this category, papers on non-concentrating solar thermal collectors and thermal storage are discussed.

21.3. Flat-plate and low-concentrating collectors

A special issue of Solar Energy includes papers on new concepts and testing methodologies for flat-plate solar collectors. Low-cost antireflective covers made with porous media and by subwavelength surface relief structures embossed in sol-gel materials improve solar transmittance by 6% [23T]. Several papers address improved absorbers. Colored absorbers intended to better integrate with buildings were evaluated in [33T]. The behavior of selective surfaces is the subject of [20T,26T,32T]. A procedure for accelerated life testing of absorber surfaces developed by the International Energy Agency is presented in [21T].

A critical review and comparison of nine dynamic test methods for flat-plate collectors is given by [29T]. [30T,31T] model the effects of various environmental and geometrical parameters on the performance of unglazed water film collectors. Kumar and Prasad [27T] investigate heat transfer enhancement due to the use of twisted tape inserts in traditional water flat-plate collector tubes. Experimental results include heat transfer rates and pressure drop. The effect of dust on transmittance of low-density polyethylene glazing is measured by [28T]. Tsilingiris [35T] proposes a polymer absorber concept for solar water heating. Vieira et al. [37T] present a semi-empirical approach to determine the void fraction in boiling collectors. Two prototype CPC collectors with flat bifacial absorbers were tested by Tripanagnostopoulos [34T]. Maximum efficiency was 0.71 with a stagnation temperature of 180 °C.

Collectors for heating air are discussed by Gao et al. [22T], Hegazy [24T,25T], and Verma and Prasad [36T]. Based on a numerical model, Gao et al. [22T] present geometric arrangements that most effectively suppress natural convection heat loss from a cross-corrugated absorber. Hegazy [24T] estimates the optimum channel geometry for collectors with flow over the absorber and on both sides of it. In a separate paper [25T], he extends the analysis to collectors that combine photovoltaic cells and air heating. Heat transfer and pressure drop characteristics of roughened absorbers are expressed in terms of a dimensionless roughness Reynolds number by Verma and Prasad [36T].

21.4. Water heating

The use of polymeric materials in solar water heating systems is considered in [39T,41T,43T]. Raman [43T] and Liu [41T] evaluate polymers for possible use as heat exchangers and analyze their effect of overall heat transfer rates. Janjai [39T] models a plastic solar collector installed on a hotel in Almeria, Spain.

Kalogirou [40T] uses an artificial neural network to model the long-term performance of 30 water heating systems in Greece. A successful project to provide hot water to a correctional facility in Arizona is discussed by May et al. [42T]. Wang [44T] tests a new hybrid water heater and adsorption icemaker.

Water heating for maintaining the temperature of a biogas reactor is evaluated in [38T].

21.5. Space heating and cooling

Papers that address solar air collectors are presented in the section on flat-plate collectors (see the discussion of [22T,24T,25T,36T]). This section presents papers on heat pump and refrigeration systems.

Ground source heat pumps systems are the subject of [47T] and [50T]. Chiasson et al. [47T] describe the de-

velopment and use of a model of a hydronic pavement heating system which is a supplemental heat rejector for a commercial building heat pump system. Kaygusuz [50T] presents limited data and a model of a specific system operated over one heating system.

Gordon and Ng [49T] discuss the performance improvements in absorption cooling made possible by recent advances in solar fiber-optic mini concentrator systems and solar-fired gas micro-turbines. Alizadeh [45T] models two regenerative chillers and compares COPs. Boubakri et al. [46T] predict ice production in an adsorptive icemaker as a function of component size. Enibe Iloje [48T] analyse heat and mass transfer in a CaCl₂ pellet – NH₃ system. Measured heat transfer data obtained for saturated nucleate boiling of water/ammonia, ammonia/lithium nitrate, and water/lithium bromide indicate that average heat transfer is greatest in the ammonia/water mixture [51T]. The use of metal wire gauze coated with zeolite to improve heat and mass transfer in the solar collector is proposed to increase COPs in solar adsorption heat pumps [52T]. Wijesundera [53T] models a solar adsorption system with an idealized three heat reservoir cycle and suggests that this method provides realistic limits and trends for cooling capacity and COP. Zhang [54T] presents a 3-D non-equilibrium model of heat and mass transfer in the adsorbent. With some modification the model can be used for system optimization.

21.6. Storage

Most papers in this section address latent heat storage. Storage in building components (e.g. walls and floors) is discussed in Buildings. Models of solid–liquid phase change are presented by [55T] for a paraffin wax–air spiral unit, [57T] for a horizontal elliptic cylinder, and [56T] and [60T] in cylindrical tubes. Kiatsirirot et al. [61T] develop an empirical expression to evaluate the volumetric heat transfer coefficient for solidification of thiosulphate pentahydrate. Experimental data and a model of temperature and void distributions in thermal storage canisters for heat receivers of solar power systems are presented in [59T] and [62T].

The sole sensible heat storage paper discusses soils up to 90 °C [58T].

21.7. Solar desalination

Papers in this section are restricted to solar distillation. Most present models and optimization of specific solar still designs based on traditional concepts [63T, 65T,68T–70T]. Mandani et al. [66T] model an evaporation process combined with a lithium bromide water absorption heat pump. Experimental data are presented in [64T] and [67T].

21.8. Cooking

The international standard for testing solar cookers is presented in [71T].

21.9. Waste treatment

Although only two papers appear in this review, there is increasing interest in the use of solar energy to treat waste. One method is photocatalytic destruction. Ajona [72T] report on the on-going efforts to commercialize the technology and provide an economic analysis of a one-sun compound parabolic concentrator (CPC) system. Nakamura [73T] considers a different technology to remove non-aqueous phase liquids, hazardous metals and radionuclides from the ground. Concentrated solar energy is transmitted to the contaminated site by optical fibers. Wastes are removed by soil vapor extraction.

21.10. Solar ponds

The archival literature contains increasingly fewer papers in this area. In 2000, two papers appeared. [75T] gives a critical review of the empirical and theoretical equations describing evaporation rates from large free water surfaces. Rivera [74T] conducted experiments to simulate the heat input of a solar pond to an absorption heat transformer.

21.11. Buildings

This section includes papers on characterization of energy consumption, and heat transfer in walls, roofs, floors, and glazings.

Models to estimate building heat and cooling loads continue to be refined. Rees [97T] presents a qualitative comparison of the ASHRAE heat balance method to the radiant time-series method and the admittance method used in the UK. Anderson [78T] describes a dynamic building stochastic model and uses it to model a residential building. Li [93T] describes a procedure for calculating hourly solar gain factors for horizontal and vertical surfaces. The method is used for the City University of Hong Kong and compared to the ASHRAE clear sky approach.

Other modeling efforts address specific building components. A 3-D transient model of a lattice solar heating wall is used to analyze the sensitivity of performance to structural parameters and to compare performance to that of a Trombe wall [87T]. The thermal dynamics of a phase change material wallboard subject to diurnal temperature variations is examined in [95T]. Studies of floors consider steady periodic conduction in

slab floors [85T] and the influence of solar radiation and floor covering on floor temperature and energy consumption in floor heating systems [79T]. A parametric study of the effects of shingle absorptivity, radiant barrier emissivity, ventilation flow rate and roof slope on the performance of radiant barriers is based on a heat balance model [94T]. Experimental study of heat transfer processes in passive finned wall is presented by Bilgen [81T].

There is growing interest in integrating photovoltaics (PV) into building design. Brinkworth [83T] presents a simplified method to estimate mass flow rates in naturally ventilated PV cladding. Yang [100T] examines heat transfer across a PV wall and predicts cooling loads contributed by such walls. An optical analysis of concentrating covers for building integrated PV is used to determine optimum tilt angles and to compare performance to flat PV covers [101T]. Multi-functional facades consisting of a transparent glazing and an opaque PV section are modeled and optimized for European locations [99T].

Many papers in the building area address coatings for glazing and other window treatments. New developments in films and coating used in switchable windows are reported in [89T–91T]. Alvarez [76T] considers transient 2-D heat transfer in a cavity with one wall with a solar control coating. Measured optical properties of a thin holographic optical element indicate that the visible light is split from the infrared, thus providing a means of separately controlling daylighting and solar gain [82T]. The angular dependence of total solar transmittance is modeled for multiple pane and coated windows [88T]. An apparatus and methodology to evaluate thermal performance of glazing are presented in [77T]. Leftheriotis [92T] also presents a method of measurement of overall heat transfer characteristics of building components. The overall heat transfer coefficients of single and double paned windows fitted with a long wave high reflectivity venetian blind are measured [86T]. Baker [80T] measured heat exchange of a double paned window used to preheat room air. Total reflectance and transmittance of glass coated with a paint made of silica particles coated by titania and then dispersed in polymeric binder were measured [98T]. The authors suggest the pigments be useful for sunscreens or foils for daylighting and radiative cooling.

Daylighting with light pipes is modeled by Chirattananon [84T]. Performance of six light pipes was measured in three building areas [96T].

21.12. High-temperature applications

High-temperature solar thermal applications require use of concentrated solar energy. Uses include electricity generation, thermochemical reactors and industrial

process heat. Papers address processes as well as system components such as heliostats, concentrators, and receivers/reactors.

Studies of concentrators include presentation of a design method for a two stage ultra flat non-imaging compact 2-D device [104T]; accelerated measurement of the long-term optical properties of aluminized reflector materials; and testing of a new rectangular cross-section secondary concentrator at the Weizmann Institute in Israel [106T] [114T]. Mills [110T] evaluates Fresnel reflectors for large-scale tower-based solar thermal electricity plants and by Larbi [108T] for operation in fixed aperture mode for medium temperature processes (200–300 °C). An approach to optimize reflector shapes for non-tracking cylindrical absorbers and reflectors is presented in [111T]. Kribus and co-workers at the Weizmann Institute consider several approaches to using optical fibers for power generation systems [107T]. Heat losses from two dish-type receivers at the Korea Institute of Energy Research are analyzed in [112T].

Theoretical papers on heat engines address factors affecting optimum power and efficiency of a Stirling cycle [103T] and the upper limit on efficiency of cyclic heat engines [113T].

Solar thermochemical processes continue to gain attention. Coal gasification is the topic of [102T] and [109T]. Belghit [102T] models heat and mass transfer in a moving chemical bed reactor. Matsunami [109T] conducted experiments to evaluate bubbling carbon dioxide through a molten salt storage medium.

Other topics related to high-temperature solar applications include solar thermal propulsion for satellites, orbit-to-orbit transfer systems and launch vehicles [105T] and solar power plant chimneys [115T]. For space applications, solar concentrators are used to achieve temperatures greater than 2200 K in compact absorbers. The heat is transferred to flowing hydrogen to produce high-energy thrust or to thermionic or alkali metal thermoelectric converters to generate electricity. The paper on solar chimney power plants models compressible flow through chimneys as tall as 1500 m [115T].

22. Plasma heat transfer and magnetohydrodynamics

22.1. Fundamental investigations on plasma heat transfer

Two publications deal with determination of plasma properties. Capitelli et al. [3U] present a model for collision integrals for species in air over a wide temperature range, to be used for calculations of transport properties. Murphy [6U] presents a review of eight different methods to calculate diffusion in thermal plasmas, and concludes that the self-consistent effective binary diffu-

sion coefficient approach is the most accurate. The effect of inserting solid or porous material into an electrical discharge has been modeled by Sawicki and Krouchinin [9U], and relations between the electrical characteristics and the fluid dynamics and the geometries of the discharge are presented. A model of a turbulent plasma jet is presented by Liu et al. [4U], and the results are shown as dimensionless temperature and velocity distributions. Another model considers the flow of a plasma over an array of particles [10U], and the effect of varying lateral and longitudinal spacing of the particles on the heat transfer is shown.

A model of the cathode region of a dc glow discharge is presented by Arslanbekov [1U] and the results show that a non-local treatment is necessary for prediction of the power dissipation. Another model of a glow discharge uses a Monte Carlo method to describe the energy transfer between the different species, and the effect on the heating of the neutral gas atoms is presented [2U]. A model of a ‘Glidarc’, a discharge traveling between diverging electrode rails, uses a simplified approach in which the arc is modeled as a hot wire cooled by a cross-flow of air [8U]. A couple of papers consider the effects of a corona discharge on the heat transfer [5U] and on the pressure drop in a tube flow [7U]. The heat transfer enhancement was determined theoretically using a large eddy simulation approach, and experimentally, and Nusselt number enhancements of up to a factor of 3.4 have been found [5U]. The study of the tube flow concentrated on experimentally determining the effect of different electrode geometries (wire and concentric tube, two parallel wires) [7U].

22.2. Specific applications

Modeling of plasmas and plasma reactor configurations as they appear in specific applications continue to find much interest. A chart which could be used for control of a plasma spray process has been developed by Ang et al. [14U] who used a commercial fluid dynamics code to compute the state of spray particles in the jet. In another paper related to plasma spraying, plasma sprayed boron carbide coatings were evaluated for their ability to withstand periodic high-heat loads [15U], and good survival rates have been found for films with a thickness of less than 150 μm which were exposed to 1000 cycles of 7.5 MW/m². Two papers from the same group deal with models of the fluid flow and heat transfer in a dc electric arc furnace [13U] including the magnetic stirring effects in molten material [12U]. For a similar reactor arrangement but with silica as the material serving as the anode for the transferred arc, Ad-dona et al. [11U] model the temperature and flow fields and the silica evaporation rates, with the objective to identify an efficient route to produce fumed silica. The

different transfer modes in gas metal arc welding have been mapped by Scotti [19U] as function of gas flow, weld current and arc length using high-speed videography.

Several papers deal with space related applications. Herdrich et al. [16U] describe an inductively coupled plasma torch operating at 180 kW with argon which is used for reentry simulation. A model description of this torch is presented by Lenzner et al. [18U] giving the energy fluxes at low pressure. A characterization of a pulsed plasma thruster where the discharge takes place in a Teflon cavity is reported by Keidar et al. [17U].

22.3. Magnetohydrodynamics

Effects of magnetic fields on fluid dynamics and heat transfer continue to be an inexhaustible source of topics for modeling approaches. Three papers deal with MHD flows along a vertical, semi-infinite flat plate, with Abo-Eldahab and El-Aziz [20U] concentrating on free convection under strong magnetic field conditions, Kim [27U] describing the unsteady flow in the boundary layer of a moving porous plate with variable suction, and Singh and Singh [29U] giving an analytical solution for the laminar boundary layer of a steadily moving porous plate. Two further papers treating the boundary layers of semi-infinite plates are describing the effect of varying surface temperature [31U], and the effects of chemical reactions and species concentration gradients [22U]. Flow past a cylinder is described in several papers, with Yih [32U] investigating the effect of blowing or suction on natural convection over a horizontal cylinder, Ganesan and Rani [25U] describing the unsteady free convection for flows past a vertical cylinder, and Mansour et al. [28U] looking at the heat and mass transfer in the boundary layer of a circular cylinder when a micropolar fluid is used. Vempaty et al. [30U] describe the flow in a rotating annulus with a radial temperature gradient, and Ghosh and Bhattacharjee [26U] present solutions for a rotating flow in a parallel plate channel and a Hall current for an inclined applied magnetic field.

A 3-D model presented by Fujisaki et al. [24U] describes the liquid metal flow under the influence of magnetic stirring and include solidification of the material, and the model has been applied to describe the continuous casting process. Eckert et al. [23U] give experimental results of the liquid metal flows under the influence of different applied magnetic fields, obtained through injection of gas bubbles and measuring the local void fraction using resistivity probes. In another experimental effort, free convection effects in the presence of magnetic fields are used for thermophoretic separation of ultrafine particles in a ferrofluid, and the Soret effect has been investigated by measuring the particle separation on a thermodiffusion column [21U].

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